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(54) Title: PROCESS FOR THE RECOVERY OF ORGANIC ACIDS FROM AQUEOUS SOLUTIONS

(57) Abstract: A process for recovering a desired organic acid from a solution includes the steps of: providing an aqueous solution including at least one desired organic acid or its acid anion; adjusting the proton concentration in the aqueous solution to a desired level, with the desired proton concentration being selected, at least in part, by the amount of available protons needed to associate with the acid anions of the desired organic acid(s) to be recovered and/or acid anions that are weaker than the desired organic acids; and recovering at least a portion of the at least one desired organic acid from the aqueous phase. The desired proton concentration can be based on the amount of available protons being greater than, less than or substantially equal, to the amount of protons needed to associate with the anion of the desired organic acid(s) and acid anions that are weaker than the desired organic acid(s). Specific examples of suitable organic acids include, but are not limited to, ascorbic, succinic, tartaric, glyconic, gulonic, citric, lactic, malic, maleic, acetic, formic, gluconic pyruvic, propionic, butyric, itaconic acids and mixtures thereof. One embodiment of the present invention relates to the recovery of 2-keto-L-gulonic acid (KLG) from aqueous solutions such as fermentation baths.

## PROCESS FOR THE RECOVERY OF ORGANIC ACIDS FROM AQUEOUS SOLUTIONS

## BACKGROUND OF THE INVENTION

## Acknowledgments

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## Field of the Invention

The present invention relates to an improved method for recovering of organic acids, and in particular degradation-sensitive organic acids, from a solution.

## Background of the Invention

It is often necessary to recover organic acids from solution. To this end, solutions containing organic acids can originate from a variety of chemical reactions and biological processes such as fermentation processes.

A typical approach to dealing with acid recovery involves the protonation of the carboxylate or salt form of the acid to reach a desired pH level.

For example, a process for the manufacture of syringic acid is taught in U.S. Patent No. 4,191,841 in which an aqueous solution containing the double alkali salt of the acid is acidified with a strong acid such as hydrochloric or sulfuric acid followed by crystallizing the carboxylic acid product. The amount of strong acid addition is that sufficient to bring the solution pH to 3.

U.S. Patent No. 4,202,828 describes a process to recover naphthoquinone and phthalic acid from a gas stream with an aqueous solvent formed by recycling the neutralized filtrate from naphthoquinone extraction and phthalic acid crystallization.

The filtrate is treated with a base to a pH of 1.2 to 2.5, preferably 1.5 to 2.2, to

- 5     neutralize only sulfuric acid and maleic acid byproducts without neutralizing unrecovered phthalic acid.

Acidification with hydrochloric acid to recover 3,6-dichloropicolinic acid from an aqueous solution of its salts in the process taught in U.S. Patent No. 4,334,074. Once again, pH is used to determine the level of acidification.

- 10            Recovery of carboxylic acids, especially N-acetyl-DL-phenylalanine carboxylic acid, made via carbonylation using cobalt carbonyl catalyst is taught in U.S. Patent No. 4,699,999. After removal of cobalt salt and any organic phase, the carboxylic acid is recovered from the aqueous phase by precipitating it with acids, especially mineral acids such as hydrochloric, sulfuric, or phosphoric acid, with the amount of acid  
15     addition based on a target pH of 1.

- The recovery of N-methyliminodiacetic acid from an aqueous solution containing its disodium salt is described in U.S. Patent No. 5,159,110. In this process, the solution is acidified using sulfuric acid and concentrated to precipitate sodium sulfate. Acidification is controlled by solution pH, with a target of approximately 2, the  
20     isoelectric point of the carboxylic acid.

- Crystallization recovery of a dicarboxylic acid from an aqueous solution containing its disodium salt is also taught in U.S. Patent 5,202,475. In this case the organic acid is 1,3- or 1,4-cyclohexanedicarboxylic acid, protonation is with hydrochloric or sulfuric acid, and the precise control of the acidification process via  
25     solution pH is again emphasized with preferred targets of 2.8 and 2.6 for the 1,4- and 1,3- isomers, respectively.

- The recovery of hydoxycholic acid from swine bile is taught in U.S. Patent No. 5,349,074. After isolation of the acid from other biliary acids and bile components as its magnesium salt, the solid hydoxycholic acid magnesium salt is suspended in an ethyl acetate aqueous solution and acidified with a mineral acid to produce the acid  
30     form. Solution pH is used to control acidification with a desired pH of 1 to 3.

The preparation of bis(amidocarboxylic acids), especially N,N'-terephthaloyl-di(6-aminocaproic acid), under basic conditions is described in U.S. Patent No. 5,410,076 in which the product is recovered by selective precipitation. Sulfuric acid

5 was used to lower the pH and precipitate the organic acid with a pH of between about 5.5 and 6.5 disclosed as providing a highest purity.

An enzymatic method for producing L-aspartic acid from maleic acid is taught in U.S. Patent No. 5,741,681 in which the reactions occur with the acids in their ammonium salt forms. Acidification to an isoelectric point of L-aspartic acid of 2.8 is  
10 disclosed as providing an improved recovery.

This reliance on pH for preformation is also prevalent in the context of organic acid recovery from fermentation broths.

For example, the production of lactic acid by fermentation followed by recovery  
15 utilizing extraction is described in U.S. Patent No. 4,771,001. Prior to extraction the fermentation broth is acidified to a desired pH level.

The recovery of lactate esters and lactic acid from fermentation broth is described in U.S. Patent No. 5,210,296 where the lactate salts are acidified in the presence of an alcohol of 4-5 carbon atoms. A strong acid such as sulfuric acid is  
20 added until the pH is between 1.0 and 1.6.

A process for recovering organic acids, especially lactic acid, from aqueous solutions such as fermentation broth is taught in U.S. Patent No. 5,426,219 in which the solution is acidulated prior to extraction. Mineral acid is used to bring the pH between 1 and 4.5 before and during extraction.

25 Despite its widespread use, pH-based techniques have not proven to be consistently effective or even predictable.

For example, in those cases where the acid form of the organic compound is less soluble than the salt form, the desired carboxylic acid may be selectively precipitated by the addition of a stronger acid having a larger acid dissociation constant or smaller ( $pK_a$ ) than the desired product. In certain cases, increasing this acidification  
30 reduces the solubility of the organic acid and can improve recovery.

However, in other cases, the desired acid decomposes in the presence of a strong acid. In such cases, recovery may actually decrease upon acidification despite the reduced solubility of the acid. The presence of organic or inorganic impurities only  
35 serves to further complicate the recovery process. For example, such impurities may

5 dissociate into cationic and anionic components, they can either compete for protons with the carboxylic acid or may donate protons into the process. Neither result is desirable.

That is, the competition for protons effectively reduces recovery of the desired organic acid while donating protons into the process can cause decomposition of the  
10 desired acid. Moreover, while the level of such impurities is typically small relative to the desired organic acid, such impurities can become concentrated during the process, thus, further magnifying their effect.

In light of the foregoing, it is clear that the existing protonation techniques are ineffective to consistently remove desired organic acids from aqueous solutions.

15 A second problem relates to the presence of anions other than that associated with the acid to be recovered. It is recognized that in the recovery of organic acids from an aqueous solution, the concentration of other anions present in the solution can strongly influence the effectiveness of the recovery process. Because of this, the art has looked towards removing the undesirable anions-as well as adjusting the solution pH-in  
20 attempting to improve the recovery process. The ion exchange technique has been employed but is equally ineffective.

In this regard, the carboxylate or salt form of the desired acid may be converted to the acid form by treating the aqueous solution with a hydrogen or free-acid form of a cation exchange resin. While this ion exchange technique may remove most, if not all,  
25 of the inorganic cations from the aqueous solution, it will also introduce its own set of problems.

For example, the resin will also protonate other anions in the solution. As was the case above, this can lead to detrimental effects. In particular, the resultant impurity acids, whether organic or inorganic in nature, are often stronger than the desired  
30 organic acid and thus may lead to decomposition of the desired acid. The ion exchange process may further dilute the solution leading to a still further decrease in recovery.

Accordingly, the need still exist for a process for which effectively recovers a desired organic acid, and in particular, a degradation-sensitive organic acid.

One organic acid of particular interest to the inventors is 2-keto-L-gulonic acid  
35 (KLG). To this end, techniques for the recovery of 2-keto-L-gulonic acid are also

5 recognized in the art. However, existing techniques for the recovery of KLG are faced with a variety of problems in addition to the pH and ion-exchange problems discussed above.

For example, many of these techniques, such as those described in U.S. Patent Nos. 2,421,611 and 2,421,612, teach crystallization recovery of this acid in its alkali or  
10 alkaline earth salt form followed by conversion to the acid form by treatment with an acid such as sulfuric. Such processes introduce a variety of problems insofar as yet another crystallization step is required to separate the 2-keto-L-gulonic acid from the aqueous acidification media for subsequent conversion steps such as esterification.

In addition, it is an art recognized belief that, in the production of a solid 2-keto-  
15 L-gulonic acid product, it is necessary to treat the aqueous solution with an anion exchange resin prior to recovery of the carboxylic acid using crystallization or extraction. See, for example, U.S. Patent Nos. 4,990,441 and 5,202,476.

Thus, the need is particularly great for an improved process for the recovery of KLG from aqueous solutions such as fermentation broths.

20

### SUMMARY OF THE INVENTION

The present invention is based, at least in part, on the surprising discovery that the optimum solution composition to recover desired organic acids cannot be effectively determined by pH measurements-with or without the knowledge of the  
25 concentration of the organic acid in the solution.

Instead, the inventive process involves adjusting the proton level in the aqueous phase to a desired proton concentration where the proton concentration is selected, at least in part, relative to the amount of protons needed to associate with the organic acid to be recovered and the acid anions that are weaker than the organic acids to be  
30 recovered.

The present invention is based, at least in part, on the further surprising discovery that optimizing recovery of the desired acid does not require the removal of other anions from the solution. Accordingly, the inventive method can be effectively employed for separating a variety of acids from aqueous environments.

5 One aspect of the invention relates to a process for recovering a desired organic acid from a solution comprising the steps of:

- (a) providing an aqueous solution including at least one desired organic acid or its acid anion;
- (b) adjusting the proton concentration in the aqueous solution to a desired level,  
10 with the desired proton concentration being selected, at least in part, by the amount of available protons needed to associate with the acid anions of the desired organic acid(s) and/or acid anions that are weaker than the desired organic acids; and
- (c) recovering at least a portion of the at least one desired organic acid from the  
15 aqueous phase.

In this regard, the desired proton concentration can be based on the amount of available protons being greater than, less than or substantially equal, to the amount of protons needed to associate with the anion of the desired organic acid(s) and acid anions that are weaker than the desired organic acid(s).

20 Specific examples of suitable organic acids include ascorbic, succinic, tartaric, glyconic, gulonic, citric, lactic, malic, maleic, acetic, formic, pyruvic, propionic, gluconic, butyric, itaconic acids and mixtures thereof.

One embodiment of the present invention relates to the recovery of 2-keto-L-gulonic acid (KLG) from aqueous solutions such as fermentation baths.

25

#### BRIEF DESCRIPTION OF THE DRAWINGS

Figure 1 illustrates the problems associated with improper protonation of the solution during the recovery process;

Figure 2 illustrates that decrease in solubility associated with increasing  
30 protonation; and

Figure 3 illustrates the increase in ascorbic acid in mother liquor with increasing protonation.

## 5 DETAILED DESCRIPTION OF THE PREFERRED EMBODIMENTS

As discussed above, the present invention relates to a method for recovering organic acids and in particular, degradation-sensitive organic acids from a solution, preferably an aqueous solution.

By "degradation-sensitive" that is referring to those organic acids that are  
10 subject to decomposition in the presence of a strong acid.

In addition, preferred organic acids include those acids where the salt form of the acid is more soluble in the solvent than the acid itself.

While any organic acid can be employed in the present invention, carboxylic acids are preferred. Specific examples of suitable organic acids that can be recovered  
15 by the inventive method include succinic, tartaric, gluconic, glyconic, citric, lactic, malic, maleic, acetic, formic, pyruvic, propionic, butyric, itaconic, ascorbic, and gulonic acids.

As discussed above, the acid can be present in the acid or anionic form thereof. It is preferred that at least a portion of the acid be present in its anionic form. Examples  
20 of suitable water ions include alkali and alkaline earth salts with specific examples of suitable counter ions including sodium, potassium and calcium. The acid can also be present in an ammonium form.

The solution can include a variety of other components including other acids, acid anions, and/or neutral organics. Specific examples of suitable acid anions include  
25 phosphates, sulfates, nitrates and chlorides among others while suitable neutral organics include sugars, aldehydes and ketones.

Moreover, other components can be present depending on the nature and use of the particular aqueous solution. For example, in employing the present invention with aqueous solutions produced from fermentation, and in particular, the recovery of 2-  
30 keto-L-gulonic acid from fermentation broths, pH can be kept neutral or near neutral by the addition of a suitable base such as aqueous ammonia, calcium carbonate, calcium hydroxide, sodium hydroxide, sodium bicarbonate, sodium carbonate or the like to convert the organic acid product to carboxylate or salt form. In addition, unreacted sugars and other feed materials can be present.



5           As discussed above, the present invention can be performed without removal of other anions from the solution.

          A first aspect of the inventive method involves a step where the proton concentration is adjusted. In this step, the aqueous solution is protonated to provide a desired proton concentration, with the desired proton concentration being based, at least  
10   in part, on the amount of protons needed to associate with the desired organic acid(s), e.g. those organic acids to be recovered, and acid anions that are weaker than the desired organic acid(s). Accordingly, this step of the process preferably involves (i) determining the state of protonation of the desired organic acid(s) and then (ii) adjusting the proton concentration to a desired level. Each of these preferred aspects of  
15   this adjustment will be discussed in detail below.

          The state of protonation of the organic acid is referenced to the equivalence point. In the context of the invention, an acid is considered to be at equivalence if the solution contains enough protons to associate with the desired organic acid and all acid anions, organic or inorganic, that are weaker than the organic acid of interest, but not  
20   enough to associate with acid anions, organic or inorganic, that are stronger than this acid.

          It is important to recognize that this definition is not meant to imply that the desired organic acid and weaker acid anions are fully associated in solution and the stronger acid anions are fully dissociated, but that there are enough protons *available* to  
25   associate with the desired organic acid anion and weaker acid anions with none left over for the stronger acid anion impurities.

          It is further recognized that the degree of proton association with the various acid anions in a given solution will be dictated by principles of chemical equilibrium. And, even at equivalence there will be some dissociation of the desired organic acid  
30   and proton association with stronger acid anions.

          The technique for determining the state of protonation is not critical to the invention. To this end, the preferred techniques include charge balance, titration, and spectroscopic methods.

          As to ionic charge balance, the state of protonation of the organic acid may be  
35   determined using compositional analysis of the aqueous solution. The concentration of

5 all species capable of forming cations or anions by dissociation should be known as well as the dissociation constants of the ionizable species present. This includes inorganic species such as alkali and alkaline earth metals generally present as cations in the solution and sulfur, phosphorus, chlorine, and the like indicative of strong acid anions. And, the concentration of the desired organic acid should be known as well as  
10 any other organic acid impurities present in significant quantities. It is especially important to know the concentration of any species capable of forming an acid stronger than the organic acid of interest as it is desirable to counter the negative charge of these anions with an inorganic cation rather than a proton.

By charge balance, the total concentration of protons in the aqueous solution is  
15 given by the following expression:

$$[H]_{\text{Total}} = \Sigma(v_i[A_i]) - \Sigma(v_j[C_j])$$

where  $[A_i]$  is the molar concentration of anionic species  $i$  with a negative charge of  $-v_i$  in its fully dissociated state and  $[C_j]$  is the molar concentration of inorganic (i.e.,  
20 excluding protons) cationic species  $j$  with a positive charge of  $+v_j$ . Again, this is not meant to imply that all of these protons are dissociated in solution. The total proton concentration  $[H]_{\text{Total}}$  simply represents the sum of associated and dissociated protons before assigning them to any particular species.

25 For example, in a solution containing the inorganic species Ca, K, Na, Mg, S, P, and Cl and the organic acid O, the total proton concentration is given by

$$[H]_{\text{Total}} = [O] + 2[S] + 3[P] + [Cl] - (2[Ca] + [K] + [Na] + 2[Mg])$$

30 This assumes that the organic acid contains a single carboxyl group, sulfur is present as the sulfate anion ( $\text{SO}_4^{2-}$ ), phosphorus is present as phosphate anion ( $\text{PO}_4^{3-}$ ), and all chlorine is inorganic chloride. Those skilled in the art can easily apply this relationship appropriately for other cases involving, for instance, multiple carboxyl groups on the organic acid or additional organic acids or inorganic electrolytes.

35 The state of protonation of the organic acid is found by determining the concentration of protons available to associate with the organic acid after assigning

5 some of this total to any acid anions present that are weaker (higher  $pK_a$ ) than the organic acid of interest. This concentration of available protons,  $[H]_{Avail}$ , is given by

$$[H]_{Avail} = [H]_{Total} - \sum(\eta_k[W_k])$$

10 where  $[W_k]$  is the concentration of weak acid anion  $k$  that remains weaker than the organic acid anion after associating with  $\eta_k$  protons. Given the molar ratio of available protons to the organic acid equals one at equivalence (for a monocarboxylic acid), this ratio may be used as a quantitative measure of the degree of protonation.

For instance, in the above example if the  $pK_a$  of the organic acid O is 2.5, the  
15 phosphate anion will associate with two protons to form the dihydrogen phosphate anion  $H_2PO_4^-$  at conditions necessary to protonate the organic acid O so

$$[H]_{Avail} = [H]_{Total} - 2[P]$$

20 for this example.

The  $pK_a$ 's of hydrochloric, the third proton of phosphoric, and both protons of sulfuric acid are lower than that of the organic acid in this case, so leaving the solution with only enough protons available for the organic acid helps prevent formation of these stronger acids. Again, even when the solution is at equivalence, there will be  
25 some dissociation of the desired organic acid and proton association with stronger acid anions. However, as the organic acid is removed from solution by extraction or crystallization, these stronger acids will donate any protons associated with their anions to the weaker organic acid.

Another method to determine the state of protonation involves the use of  
30 titration. Given the solution is at equivalence when the molar concentrations of available protons and organic acid are equal, the molar amount of protons to add (subtract) to reach equivalence,  $H_{Eq}$ , is given by

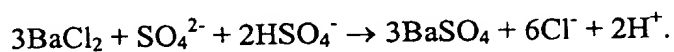
$$H_{Eq} = O - H_{Avail}$$

35 where O is the molar amount of organic acid O present and  $H_{Avail}$  is the molar amount of available protons in solution. Typically,  $H_{Eq}$  would be determined by titration with a strong acid titrant in water solvent. However, for a relatively strong organic acid like

5 2-keto-L-gulonic acid (KLG),  $H_{Eq}$  cannot be determined by titration with a strong acid in water because the organic acid anion is too weak a base to give an adequate end point.

Any solvent that is aprotic or at least a very weak acid can be employed in the titration of such organic acids. Moreover, the choice of preferred solvent is dependent  
10 on the acid in question. Specifically, dimethyl sulfoxide (DMSO) is preferred for obtaining a good end point with KLG solutions because it is aprotic and a good solvent for the titration components.

The presence of other acid or base species can complicate the titration of acid solutions. For example, in connection with KLG titration done in DMSO sulfate acts  
15 as a weak base along with the KLG anion that leads to an error in the amount of acid needed to reach equivalence. The addition of excess barium chloride before the titration eliminates problems caused by sulfate:



20 Sulfate, and interference in the titration, is removed and the proton associated with bisulfate is freed to protonate the organic acid. Therefore, only dissociated organic acid anion and other weak acid anions are titrated and the amount of acid to reach equivalence in the titration reflects the amount needed to reach equivalence in the  
25 solution.

While the addition of barium chloride provides a convenient correction for the sulfate problem in DMSO, the titration could be done without it and a correction made based on the amount of sulfate as determined by ion chromatography or another technique. Similar considerations could be made for other components present at  
30 significant concentrations. Also, for the case in which available protons exceed those needed to protonate the organic acid, the titration could be performed with a strong base, or, alternatively, a known amount of strong base added and back titrated with acid.

A second aspect of the protonation step involves adjusting the proton  
35 concentration based, at least in part, on the state of protonation of the desired organic

5 acid(s). This adjustment technique can involve one or more steps depending upon the particular organic acid to be recovered.

For example, when employing an aqueous solution containing the salt form of the desired organic acid(s), the adjustment can be performed in a single step by adding a proper amount of a strong acid. By strong acid, it is meant an acid that is strong in  
10 comparison to the organic acid being recovered. Suitable examples of strong acids for use with the preferred organic acids include hydrochloric, sulfuric, nitric and phosphoric acids.

Alternatively, a two-step process can be employed. In this embodiment, all of the acid ions, both weak and strong, can be protonated with an hydrogen or acid form  
15 of a cationic exchange resin followed by an addition of an appropriate amount of base for neutralization of the strong acids only.

Specific examples of suitable cation exchange resins include sulfonated polystyrene resins such as Ambersep 200H, Amberlite IR-118 H form, Dowex 50X2-100, 50X2-200, 50X2-400, 50X8-200, 50X8-400, HBK-530 H form, and HBK-550 H  
20 form.

Depending on a particular base employed in neutralization, the two-step process may have the advantage of eliminating inorganic salt impurities in the organic acid product by first removing all of the inorganic cations such as calcium that can form insoluble or sparingly soluble salts. Moreover, it can be superior to the use of a cation  
25 exchange resin alone in that the strong acids produced by the cation exchange are neutralized so as to avoid decomposition problems.

In an alternative embodiment relating to the two-step process, a slip stream comprising the carboxylate-containing solution can be bypassed around the cation exchange step and used to neutralize the strong acids formed therein.

30 Yet another embodiment involves a three-step protonation technique. A suitable three-step technique could include:

- (1) conversion of the bulk of the carboxylate to its acid form by treatment with a strong acid followed by removal of any precipitated salts;
- (2) protonating any remaining acid ions with the hydrogen or acid form of a  
35 cation exchange resin, and finally,

5 (3) adding an appropriate amount of base to neutralize resulting strong acids.  
Specific examples of suitable bases include sodium hydroxide and potassium  
hydroxide.

This technique can be effectively employed in processes such as those processes  
where it is important to reduce the load on the cation exchange resin in those cases  
10 where the cation forming the salt produces an insoluble or sparingly soluble inorganic  
salt upon acidification with a mineral acid, such as sulfuric acid or hydrochloric acid.

In each of the techniques, the proton concentration can be adjusted to any  
desired level based upon the state of protonation of the desired organic acid. To this  
end, it is within the scope of the present invention to both overprotonate, i.e., provide a  
15 proton concentration greater than the equivalence level, as well as underprotonate,  
depending upon the particular acid to be recovered and the aqueous solution employed.

In particular, discussed above, over protonation may lead to the decomposition  
of the organic acid during subsequent evaporation or concentration steps, while under  
protonation will leave some of the organic acid in its carboxylic form which can  
20 potentially lead to salt impurities in the organic acid product or even lower yields of the  
acid product. However, the ability to determine and employ the state of protonation  
and determining proton concentration is a key aspect of the present invention. To this  
end, in most cases it is preferred that the proton concentration be adjusted such that the  
organic acid is at its equivalence.

25 The desired proton concentration is dependent on a number of factors including  
the precise organic acids to be removed, other anions in the system and the like.

Since solubility is generally minimized at high ratios of available protons to  
organic acid, it is often preferred that the aqueous solution be overprotonated relative to  
equivalence to maximize recovery. Where overprotonation is desired, the proton  
30 concentration is preferably about 1 to about 10 % by mole greater than equivalence.

However, in certain circumstances overprotonation conditions may lead to  
decomposition of the organic acid during subsequent recovery, e.g, evaporation or  
concentration steps. In such cases, underprotonation can be preferred. In the case of  
underprotonation, preferred proton concentrations are on the order of about 1 to about  
35 10% by mole less than equivalence.

5 On the other hand, underprotonating the solution will leave some of the organic acid in its carboxylate form potentially leading to salt impurities in the organic acid product or lower yields. Optimizing recovery via crystallization requires protonating the feed such that solubility is minimized without leading to unacceptable decomposition losses.

10 Accordingly, in many cases, adjusting the proton concentration so that the organic acid is at equivalence will be optimal.

This can be demonstrated by relating the state of protonation of the feed to that of the solution remaining after significant organic acid recovery. By material balance, one can derive the following relationship between the ratio of available protons to organic acid O in the feed  $([H]_{Avail}/[O])^F$  to that in the filtrate or mother liquor  $([H]_{Avail}/[O])^{ML}$  after fractional recovery  $r$  of the acid:

$$([H]_{Avail}/[O])^{ML} = 100\% \left[ 1 - \frac{1}{(1-r)} \left( 1 - \frac{([H]_{Avail}/[O])^F}{100\%} \right) \right]$$

This equation is plotted in Figure 1 as a function of fractional recovery for feed  $[H]_{Avail}/[O]$  values from 85 to 115%. At organic acid recoveries above 85%, the protonation level in the mother liquor deviates significantly from that of the feed for initial protonations other than equivalence (i.e., 100%). These deviations will dramatically impact solubility, decomposition, and, thus, the recovery actually attainable. So, unless it is desirable to operate subsequent recovery steps at  $[H]_{Avail}/[O]$  ratios away from 100% due to solubility or decomposition concerns, the feed should be protonated to equivalence.

A preferred application for the inventive process relates to the formation of ascorbic acid and in particular, the recovery of 2-keto-L-gulonic acid.

To this end, the 2-keto-L-gulonic acid can be produced by any technique recognized within the art including fermentation, the Reichstein process and hydrolysis of diactone 2-keto-L-gulonic acid (2,3; 4,6-diisopropylidene-oxo-L-gulonic acid) monohydrate or its anhydride.

Alternatively, the inventive method can be employed with a recovery of variety of organic acids from aqueous solutions, and in particular, those aqueous solutions containing carboxylic acids discussed within the background of the invention.

5           Subsequent to adjusting the proton concentration, the desired organic acid(s) are removed from the aqueous phase. To this end, the exact method for recovery is not critical to the claimed invention in that any recovery technique recognized within the art can be employed within the present invention.

10           For example, suitable techniques involve isolation of the desired organic acid(s) by crystallizing the acid from the aqueous phase followed by at least one of filtration, centrifugation, decantation, extraction and/or spray drying.

15           The inventive method can also include recycling or reuse of various streams produced therein. For example, such a recycle can include the aqueous phase remaining subsequent to recovery which is recycled by into the starting material in order to provide for additional removal of any remaining organic acid(s).

          Moreover, the recycle stream(s) can be contacted with suitable anion or cation exchange resins prior to reintroduction into the aqueous solution.

20           The desired organic acid(s) can be employed in any art-recognized process. For example, where KLG is to be removed from an aqueous fermentation broth, the KLG can be used in the formation of ascorbic acid. Other uses for the various organic acids are well recognized in the art and as such need not be described in detail here.

25           The present invention is capable of providing a proper proton concentration in an aqueous stream containing a desired carboxylate or salt form of organic acid without the need of contacting the aqueous solution with an anion exchange resin. Moreover, this process allows for recovery of the desired acid product to be maximized during subsequent recovery steps. Finally, the present invention is capable of providing this recovery in a cost-effective manner.

30           The present invention will now be described in terms of certain specific examples. However, it should be recognized that these examples are only illustrative in nature and in no way limit the scope of the present invention.

### Examples

35           The following examples relate to the recovery of 2-keto-L-gulonic acid (KLG) from fermentation broth via crystallization. Examples 1-44 are representative of prior art methods to protonate the KLG prior to crystallization while Examples 45-70 reflect



5 proper protonation of the organic acid herein. In all cases the KLG-containing broths were prepared by aerobic fermentation of glucose and fructose feeds with a recombinant DNA organism and pH controlled to 5-6 with  $\text{Ca}(\text{OH})_2$  addition. As described in the following examples, the broths were typically acidified to pH~2 with sulfuric acid and clarified using activated carbon and filtration to remove cells, gypsum,  
10 and other inorganic salts before any additional treatments.

### Example 1

After acidification to pH~2 with sulfuric acid, carbon treatment, and microfiltration to remove cells, carbon and other solids, 3031 grams of a broth with  
15 composition given in Table 1 was subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (K, Na, and P) increased by a factor of 7.52 in the mother liquor, or filtrate, relative to that in the feed and 2312.6 grams of distillate was recovered. After vacuum filtration, a methanol wash, and drying, 361.1 grams of a 86.6 wt% pure (anhydrous  
20 basis) KLG product was recovered corresponding to 77.9% KLG recovery. The composition of the mother liquor is given in Table 2. Comparison of the ratio of available protons to KLG as determined by charge balance in the feed (87.5%) to that in the mother liquor (60.9%) reveals that the feed broth was underprotonated and became even more proton deficient as KLG was crystallized. This was also reflected  
25 by the pH increase from 1.8 in the feed to 2.08 in the mother liquor.

### Example 2

To simulate mother liquor recycle in a continuous crystallization process, 160 grams of the mother liquor from the batch crystallization described in Example 1 was  
30 combined with 2441.2 grams of the same fresh feed and subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (K, Na, and P) increased by a factor of 6.00 in the mother liquor, or filtrate, relative to that in the fresh feed and 1772.2 grams of distillate was recovered. After vacuum filtration, a methanol wash, and drying, 185.23 grams of  
35 a 85.9 wt% pure (anhydrous basis) KLG product was recovered corresponding to

5 41.8% KLG recovery. The composition of the resultant mother liquor is given in Table  
2. Given the mother liquor from Example 1 was more underprotonated than the fresh  
feed (60.9% versus 87.5%), it is not surprising that the ratio of available protons to  
KLG was even lower in this mother liquor (43.5%). This underprotonation likely  
contributed to the poor KLG recovery and illustrates the shortcomings of relying solely  
10 on pH to control acidification of the carboxylate solution.

### Example 3

After acidification to pH~2 with sulfuric acid, carbon treatment, and  
microfiltration to remove cells, carbon and other solids, the same broth used as the  
15 fresh feed in Examples 1 and 2 was further pretreated by contact with the hydrogen  
form of a cation exchange resin. The resultant broth had a composition given in Table  
1, of which 3000.5 grams was subjected to evaporative crystallization at 10°C. The  
broth was evaporated to the point at which the phosphorus concentration increased by a  
factor of 4.90 in the mother liquor, or filtrate, relative to that in the feed and 2240  
20 grams of distillate was recovered. After vacuum filtration, a methanol wash, and  
drying, 215.0 grams of a 88.1 wt% pure (anhydrous basis) KLG product was recovered  
corresponding to 52.6% KLG recovery. The composition of the mother liquor is given  
in Table 2. In contrast to Example 1, comparison of the ratio of available protons to  
KLG in the feed (112.1%) to that in the mother liquor (132.4%) reveals that the feed  
25 broth was overprotonated and became more so as KLG was crystallized. This was also  
reflected by the pH decrease from 1.8 in the feed to 0.44 in the mother liquor and the  
appearance of ascorbic acid, a byproduct of KLG decomposition, in the mother liquor  
(1.39 wt%). This example further illustrates the inadequacy of using pH as a measure  
of protonation as the fresh feed pH was the same (1.8) as in Example 1, although by  
30 charge balance the feed in Example 1 was underprotonated while in this case it was  
overprotonated.

### Example 4

To simulate mother liquor recycle in a continuous crystallization process, 423.6  
35 grams of the mother liquor from the batch crystallization described in Example 3 was

5 combined with 2440.6 grams of the same fresh feed and subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the phosphorus concentration increased by a factor of 8.63 in the mother liquor, or filtrate, relative to that in the fresh feed and 2000.7 grams of distillate was recovered. After vacuum filtration, a methanol wash, and drying, 300.88 grams of a 86.8 wt% pure (anhydrous basis) KLG product was recovered corresponding to 67.9% KLG recovery. The composition of the resultant mother liquor is given in Table 2. Given the mother liquor from Example 3 was more overprotonated than the fresh feed (132.4% versus 112.1%), it is not surprising that the ratio of available protons to KLG was even higher in this mother liquor (178.5%). KLG losses by decomposition were also higher as reflected by the increased ascorbic acid level in the mother liquor (2.28 wt%).

#### Example 5

To further simulate mother liquor recycle in a continuous crystallization process, 490 grams of the mother liquor from the batch crystallization described in Example 4 was combined with 2433.1 grams of the same fresh feed used in Examples 3 and 4 and subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the phosphorus concentration increased by a factor of 11.76 in the mother liquor, or filtrate, relative to that in the fresh feed and 2000.8 grams of distillate was recovered. After vacuum filtration, a methanol wash, and drying, 285.53 grams of a 84.5 wt% pure (anhydrous basis) KLG product was recovered corresponding to 65.2% KLG recovery. The composition of the resultant mother liquor is given in Table 2. Given the mother liquor from Example 4 was even more overprotonated than the fresh feed (178.5% versus 112.1%), it is not surprising that the ratio of available protons to KLG was yet even higher in this mother liquor (203.2%). KLG losses by decomposition were also higher as reflected by the increased ascorbic acid level in the mother liquor (2.81 wt%).

#### Example 6

After microfiltration at pH~7 to remove cells, acidification to pH~2 with sulfuric acid, carbon treatment, and filtration to remove carbon and other solids, a broth

5 was further pretreated by adding more sulfuric acid, filtration, and contact with the hydrogen form of a cation exchange resin. The additional sulfuric acid was intended to fully protonate the KLG and was based upon a  $C^{13}$  NMR measurement of the degree of proton association with KLG in the broth. The resultant broth had a composition given in Table 1, of which 3000.2 grams was subjected to evaporative crystallization at 10°C.

10 The broth was evaporated to the point at which the concentration of phosphorus increased by a factor of 6.32 in the mother liquor, or filtrate, relative to that in the feed and 2387.6 grams of distillate was recovered. After vacuum filtration, a methanol wash, and drying, 234.85 grams of a 87.4 wt% pure (anhydrous basis) KLG product was recovered corresponding to 76.9% KLG recovery. The composition of the mother

15 liquor is given in Table 2. The combination of additional sulfuric acid and cation exchange led to overprotonation as reflected by the ratio of available protons to KLG in the feed of 136.6% and it became more so as KLG was crystallized as the ratio increased to 261.4% in the mother liquor. Again, there was evidence for KLG decomposition as the mother liquor contained 2.85 wt% ascorbic acid.

20

#### Example 7

To simulate mother liquor recycle in a continuous crystallization process, 217.7 grams of the mother liquor from the batch crystallization described in Example 6 was combined with 2640.3 grams of the same fresh feed and subjected to evaporative

25 crystallization at 10°C. The broth was evaporated to the point at which the phosphorus concentration increased by a factor of 14.93 in the mother liquor, or filtrate, relative to that in the fresh feed and 2239.9 grams of distillate was recovered. The composition of the resultant mother liquor is given in Table 2. Given the mother liquor from Example 6 was more overprotonated than the fresh feed (261.4% versus 136.6%), it is not

30 surprising that both the ratio of available protons to KLG (300.2%) and ascorbic acid levels (3.14 wt%) were even higher in this mother liquor.

#### Example 8

The feed broth for this example was pretreated the same as that described in

35 Example 6 except yet even more sulfuric acid was added before cation exchange. The

5 resultant broth had a composition given in Table 1, of which 3000.4 grams was subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the phosphorus concentration increased by a factor of 6.16 in the mother liquor, or filtrate, relative to that in the feed and 2317.6 grams of distillate was recovered. After vacuum filtration, a methanol wash, and drying, 230.42 grams of a  
10 84.9 wt% pure (anhydrous basis) KLG product was recovered corresponding to 59.9% KLG recovery. The composition of the mother liquor is given in Table 2. The combination of extra sulfuric acid and cation exchange led to even greater overprotonation as reflected by the ratio of available protons to KLG in the feed of 143.8% and it became more so as KLG was crystallized as the ratio increased to  
15 329.8% in the mother liquor. Again, there was evidence for KLG decomposition as the mother liquor contained 2.0 wt% ascorbic acid.

#### Example 9

To simulate mother liquor recycle in a continuous crystallization process, 323.6  
20 grams of the mother liquor from the batch crystallization described in Example 8 was combined with 2580.1 grams of the same fresh feed and subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the phosphorus concentration increased by a factor of 10.25 in the mother liquor, or filtrate, relative to that in the fresh feed and 2189.2 grams of distillate was recovered. After vacuum  
25 filtration, a methanol wash, and drying, 242.54 grams of a 89.6 wt% pure (anhydrous basis) KLG product was recovered corresponding to 67.2% KLG recovery. The composition of the resultant mother liquor is given in Table 2. Given the mother liquor from Example 8 was more overprotonated than the fresh feed (329.8% versus 143.8%), it is not surprising that the ratio of available protons to KLG was even higher in this  
30 mother liquor (604.2%). KLG losses by decomposition were also higher as reflected by the increased ascorbic acid level in the mother liquor (3.37 wt%).

#### Example 10

To further simulate mother liquor recycle in a continuous crystallization  
35 process, 213.9 grams of the mother liquor from the batch crystallization described in

5 Example 9 was combined with 2510.3 grams of the same fresh feed used in Examples 8 and 9 and subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the phosphorus concentration increased by a factor of 8.95 in the mother liquor, or filtrate, relative to that in the fresh feed and 2121.7 grams of distillate was recovered. After vacuum filtration, a methanol wash, and drying, 242.21 grams of  
10 a 86.7 wt% pure (anhydrous basis) KLG product was recovered corresponding to 71.3% KLG recovery. The composition of the resultant mother liquor is given in Table 2. Because this broth was not concentrated by evaporation as much as that in Example 9, the ratio of available protons to KLG in the mother liquor was somewhat lower (503.1% versus 604.2%). It was clearly overprotonated, however, with 3.21 wt% of the  
15 KLG decomposition product ascorbic acid in the mother liquor.

#### Example 11

After acidification to pH~2 with sulfuric acid, carbon treatment, and microfiltration to remove cells, carbon and other solids, the same broth used as the  
20 fresh feed in Examples 1 and 2 was further pretreated by adding more sulfuric acid, filtration, and contact with the hydrogen form of a cation exchange resin. The additional sulfuric acid was beyond that required to fully protonate the KLG based upon a C<sup>13</sup> NMR measurement of the degree of proton association with KLG in the broth. The resultant broth had a composition given in Table 1, of which 3004 grams  
25 was subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the phosphorus concentration increased by a factor of 4.02 in the mother liquor, or filtrate, relative to that in the feed and 2133.4 grams of distillate was recovered. After vacuum filtration, a methanol wash, and drying, 205.27 grams of a  
30 86.5 wt% pure (anhydrous basis) KLG product was recovered corresponding to 48.1% KLG recovery. The composition of the mother liquor is given in Table 2. The combination of additional sulfuric acid and cation exchange led to overprotonation as reflected by the ratio of available protons to KLG in the feed of 141.3% and it became more so as KLG was crystallized as the ratio increased to 215.5% in the mother liquor. Again, there was evidence for KLG decomposition as the mother liquor contained 1.35  
35 wt% ascorbic acid.

5    Example 12

        To simulate mother liquor recycle in a continuous crystallization process, 590 grams of the mother liquor from the batch crystallization described in Example 11 was combined with 2610.1 grams of the same fresh feed and subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the phosphorus  
10    concentration increased by a factor of 5.90 in the mother liquor, or filtrate, relative to that in the fresh feed and 2075.2 grams of distillate was recovered. After vacuum filtration, a methanol wash, and drying, 250.66 grams of a 88.2 wt% pure (anhydrous basis) KLG product was recovered corresponding to 51.8% KLG recovery. The composition of the resultant mother liquor is given in Table 2. Given the mother liquor  
15    from Example 11 was more overprotonated than the fresh feed (215.5% versus 141.3%), it is not surprising that the ratio of available protons to KLG was even higher in this mother liquor (288.8%). KLG losses by decomposition were also higher as reflected by the increased ascorbic acid level in the mother liquor (2.12 wt%).

20    Example 13

        To further simulate mother liquor recycle in a continuous crystallization process, 680 grams of the mother liquor from the batch crystallization described in Example 12 was combined with 2450.2 grams of the same fresh feed used in Examples 11 and 12 and subjected to evaporative crystallization at 10°C. The broth was  
25    evaporated to the point at which the phosphorus concentration increased by a factor of 11.91 in the mother liquor, or filtrate, relative to that in the fresh feed and 2210.4 grams of distillate was recovered. After vacuum filtration, a methanol wash, and drying, 344.82 grams of a 82.5 wt% pure (anhydrous basis) KLG product was recovered corresponding to 69.4% KLG recovery. The composition of the resultant mother liquor  
30    is given in Table 2. The high degree of concentration by evaporation and the overprotonated feeds combined to lead to a very high ratio of available protons to KLG of 606.4% and a high ascorbic acid level of 4.87 wt% in this mother liquor.

#### 5    Example 14

After microfiltration at pH~7 to remove cells, acidification to pH~2 with sulfuric acid, carbon treatment, and filtration to remove carbon and other solids, a broth was further pretreated by contact with the hydrogen form of a cation exchange resin. The resultant broth had a composition given in Table 1, of which 3000.1 grams was  
10 subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the concentration of phosphorus increased by a factor of 5.03 in the mother liquor, or filtrate, relative to that in the feed and 2236.7 grams of distillate was recovered. After vacuum filtration, a methanol wash, and drying, 100.56 grams of a  
15 89.4 wt% pure (anhydrous basis) KLG product was recovered corresponding to 36.1% KLG recovery. The composition of the mother liquor is given in Table 2. The cation exchange led to slight overprotonation as reflected by the ratio of available protons to KLG in the feed of 112.7% and it became only slightly more so during crystallization as the ratio increased to 119.8% in the mother liquor. KLG decomposition at these  
20 relatively mild conditions was minimal as reflected by the low ascorbic acid level of 0.53 wt% in this mother liquor. Again, pH was a poor measure of protonation as it decreased from 1.8 in the feed to 0.4 in the mother liquor much like Example 3 while both overprotonation of the mother liquor as determined by charge balance (119.8% versus 132.4%) and KLG decomposition as indicated by ascorbic acid level (0.53 versus 1.39 wt%) were lower in this example.

25

#### Example 15

To simulate mother liquor recycle in a continuous crystallization process, 511.6 grams of the mother liquor from the batch crystallization described in Example 14 was combined with 2840.2 grams of the same fresh feed and subjected to evaporative  
30 crystallization at 10°C. The broth was evaporated to the point at which the phosphorus concentration increased by a factor of 7.03 in the mother liquor, or filtrate, relative to that in the fresh feed and 2217.1 grams of distillate was recovered. After vacuum filtration, a methanol wash, and drying, 249.77 grams of a 88.9 wt% pure (anhydrous basis) KLG product was recovered corresponding to 59.7% KLG recovery. The  
35 composition of the resultant mother liquor is given in Table 2. Because the protonation



5 level of the fresh feed (112.7%) and the mother liquor feed (119.8%) were similar and the feed was not highly concentrated, the ratio of available protons to KLG in the mother liquor increased only modestly to 132.6% in this example. Likewise, the mother liquor pH (0.35) and ascorbic acid level (0.93 wt%) were indicative of only modest overprotonation.

10

#### Example 16

To further simulate mother liquor recycle in a continuous crystallization process, 741.1 grams of the mother liquor from the batch crystallization described in Example 15 was combined with 2540.1 grams of the same fresh feed used in Examples 14 and 15 and subjected to evaporative crystallization at 10°C. The broth was 15 evaporated to the point at which the phosphorus concentration increased by a factor of 9.07 in the mother liquor, or filtrate, relative to that in the fresh feed and 2137.1 grams of distillate was recovered. After vacuum filtration, a methanol wash, and drying, 206.39 grams of a 89.7 wt% pure (anhydrous basis) KLG product was recovered 20 corresponding to 49.2% KLG recovery. The composition of the resultant mother liquor is given in Table 2. Overprotonation was higher in this example than in Example 15 as indicated by the ratio of available protons to KLG in the mother liquor (146.8%), the ascorbic acid level (1.67 wt%), and the mother liquor pH (0.15).

#### 25 Example 17

After acidification to pH~2 with sulfuric acid, carbon treatment, and microfiltration to remove cells, carbon and other solids, the same broth used as the fresh feed in Examples 1 and 2 was further pretreated by adding more sulfuric acid and filtration. The additional sulfuric acid was that required to fully protonate the KLG 30 based upon a C<sup>13</sup> NMR measurement of the degree of proton association with KLG in the broth. The resultant broth had a composition given in Table 1, of which 3000 grams was subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (K, Na, Mg, and P) increased by a factor of 8.76 in the mother liquor, or filtrate, relative to that in the 35 feed and 2304.1 grams of distillate was recovered. After vacuum filtration, a methanol

5 wash, and drying, 301.58 grams of a 86.6 wt% pure (anhydrous basis) KLG product was recovered corresponding to 65.8% KLG recovery. The composition of the mother liquor is given in Table 2. The additional sulfuric acid alone led to overprotonation as reflected by the ratio of available protons to KLG in the feed of 110.7% and it became more so as KLG was crystallized as the ratio increased to 161.2% in the mother liquor.

10 This example further illustrates the shortcoming of using pH as a measure of protonation as the pH of the feed in this example was 1.41 while the pH for the feeds in Examples 3 and 14 were both 1.8 despite having similar ratios of available protons to KLG as determined by charge balance (Table 1).

#### 15 Example 18

To simulate mother liquor recycle in a continuous crystallization process, 184.1 grams of the mother liquor from the batch crystallization described in Example 17 was combined with 3000.9 grams of the same fresh feed and subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the average

20 concentration of soluble inorganics (K, Na, Mg, and P) increased by a factor of 8.03 in the mother liquor, or filtrate, relative to that in the fresh feed and 2441.5 grams of distillate was recovered. After vacuum filtration, a methanol wash, and drying, 306.81 grams of a 88.7 wt% pure (anhydrous basis) KLG product was recovered corresponding to 62.4% KLG recovery. The composition of the resultant mother liquor

25 is given in Table 2. Because the feed was a little less concentrated by evaporation as in Example 17, the ratio of available protons to KLG in the mother liquor was slightly lower (148.4% versus 161.2%) in this example.

#### Example 19

30 To further simulate mother liquor recycle in a continuous crystallization process, 466.2 grams of the mother liquor from the batch crystallization described in Example 18 was combined with 2663.1 grams of the same fresh feed used in Examples 17 and 18 and subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (K,

35 Na, Mg, and P) increased by a factor of 10.78 in the mother liquor, or filtrate, relative

5 to that in the fresh feed and 2165.3 grams of distillate was recovered. After vacuum filtration, a methanol wash, and drying, 341.85 grams of a 86.7 wt% pure (anhydrous basis) KLG product was recovered corresponding to 64.8% KLG recovery. The composition of the resultant mother liquor is given in Table 2. Consistent with the higher degree of concentration by evaporation, overprotonation was somewhat higher  
10 in this example than in Examples 17 and 18 as indicated by the ratio of available protons to KLG in the mother liquor (172.7%).

#### Example 20

After microfiltration at pH~7 to remove cells, acidification to pH~2 with  
15 sulfuric acid, carbon treatment, and filtration to remove carbon and other solids, a broth was further pretreated by adding more sulfuric acid and filtration. The additional sulfuric acid was that required to fully protonate the KLG based upon a C<sup>13</sup> NMR measurement of the degree of proton association with KLG in the broth. The resultant broth had a composition given in Table 1, of which 3000.3 grams was subjected to  
20 evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (K, Na, Mg, and P) increased by a factor of 8.77 in the mother liquor, or filtrate, relative to that in the feed and 2302.1 grams of distillate was recovered. After vacuum filtration, a methanol wash, and drying, 250.25 grams of a 84.4 wt% pure (anhydrous basis) KLG product was recovered  
25 corresponding to 57.0% KLG recovery. The composition of the mother liquor is given in Table 2. The additional sulfuric acid alone led to overprotonation as reflected by the ratio of available protons to KLG in the feed of 110.0% and it became more so as KLG was crystallized as the ratio increased to 151.1% in the mother liquor. Decreasing pH from 1.44 in the fresh feed to 0.63 in the mother liquor was also indicative of this  
30 increasing acidification.

Comparison of these results with those from Example 17 reveals that despite starting from similar protonation levels, concentrating by the same factor, and obtaining the same KLG solubility in the mother liquor, both KLG recovery and mother liquor protonation were lower in this example than in Example 17. This reflects the lower

- 5 KLG concentration in the pretreated feed for this example and can be rationalized using simple mass-balance models.

#### Example 21

- To simulate mother liquor recycle in a continuous crystallization process, 260.9  
10 grams of the mother liquor from the batch crystallization described in Example 20 was combined with 3000.1 grams of the same fresh feed and subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (K, Na, Mg, and P) increased by a factor of 11.38 in the mother liquor, or filtrate, relative to that in the fresh feed and 2400 grams of  
15 distillate was recovered. After vacuum filtration, a methanol wash, and drying, 323.37 grams of a 86.6 wt% pure (anhydrous basis) KLG product was recovered corresponding to 65.7% KLG recovery. The composition of the resultant mother liquor is given in Table 2. The overprotonated feed and relatively high degree of concentration led to a higher ratio (176.5%) of available protons to KLG and lower pH  
20 (0.57) in this mother liquor compared to that from Example 20.

#### Example 22

- To further simulate mother liquor recycle in a continuous crystallization process, 360 grams of the mother liquor from the batch crystallization described in  
25 Example 21 was combined with 2490 grams of the same fresh feed used in Examples 20 and 21 and subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (K, Na, Mg, and P) increased by a factor of 12.25 in the mother liquor, or filtrate, relative to that in the fresh feed and 2090.9 grams of distillate was recovered. After vacuum  
30 filtration, a methanol wash, and drying, 299.46 grams of a 84.8 wt% pure (anhydrous basis) KLG product was recovered corresponding to 67.3% KLG recovery. The composition of the resultant mother liquor is given in Table 2. Consistent with the slightly higher degree of concentration by evaporation, overprotonation was a little higher in this example than in Examples 20 and 21 as indicated by the ratio of available  
35 protons to KLG in the mother liquor (181.0%).

5     Example 23

After microfiltration at pH~7 to remove cells, acidification to pH~2 with sulfuric acid, carbon treatment, and filtration to remove carbon and other solids, the same broth used to prepare the fresh feeds in Examples 6-10, 14-16, and 20-22 was crystallized without further pretreatment. This underacidified broth had a composition  
10     given in Table 1, of which 3000 grams was subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (K, Na, Mg, and P) increased by a factor of 7.73 in the mother liquor, or filtrate, relative to that in the feed and 2225.6 grams of distillate was recovered. After vacuum filtration, a methanol wash, and drying, 237.27 grams of a  
15     82.0 wt% pure (anhydrous basis) KLG product was recovered corresponding to 53.5% KLG recovery. The composition of the mother liquor is given in Table 2. Comparison of the ratio of available protons to KLG as determined by charge balance in the feed (89.3%) to that in the mother liquor (68.6%) reveals that the feed broth was underprotonated and became even more proton deficient as KLG was crystallized.

20

Example 24

To simulate mother liquor recycle in a continuous crystallization process, 225.8 grams of the mother liquor from the batch crystallization described in Example 23 was combined with 2800.6 grams of the same fresh feed and subjected to evaporative  
25     crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (K, Na, Mg, and P) increased by a factor of 9.77 in the mother liquor, or filtrate, relative to that in the fresh feed and 2263.9 grams of distillate was recovered. After vacuum filtration, a methanol wash, and drying, 307.96 grams of a 80.9 wt% pure (anhydrous basis) KLG product was recovered  
30     corresponding to 60.9% KLG recovery. The composition of the resultant mother liquor is given in Table 2. The increased concentration factor and addition of even further underprotonated mother liquor to the fresh feed led to a greater degree of proton deficiency in this example as reflected by both the ratio of available protons to KLG (63.0% versus 68.6%) and pH (2.18 versus 2.14) when compared to Example 23.

35

5    Example 25

To further simulate mother liquor recycle in a continuous crystallization process, 234.2 grams of the mother liquor from the batch crystallization described in Example 24 was combined with 2800.1 grams of the same fresh feed used in Examples 23 and 24 and subjected to evaporative crystallization at 10°C. The broth was  
10    evaporated to the point at which the average concentration of soluble inorganics (K, Na, Mg, and P) increased by a factor of 10.32 in the mother liquor, or filtrate, relative to that in the fresh feed and 2250 grams of distillate was recovered. After vacuum filtration, a methanol wash, and drying, 340.16 grams of a 81.2 wt% pure (anhydrous basis) KLG product was recovered corresponding to 66.3% KLG recovery. The  
15    composition of the resultant mother liquor is given in Table 2. Again, this mother liquor was underprotonated as reflected by both its ratio of available protons to KLG (63.4%) and pH (2.23).

Example 26

20    The same broth used as the fresh feed in Examples 23-25 was further pretreated by adding more sulfuric acid, filtration, and contact with the hydrogen form of a cation exchange resin much like the fresh feed used in Examples 6 and 7. The additional sulfuric acid was intended to fully protonate the KLG and was based upon a C<sup>13</sup> NMR measurement of the degree of proton association with KLG in the broth. The resultant  
25    broth had a composition given in Table 1, of which 3000 grams was subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (K, Na, and P) increased by a factor of 5.76 in the mother liquor, or filtrate, relative to that in the feed and 2224.1 grams of distillate was recovered. After vacuum filtration, a methanol wash, and drying, 211.06 grams of  
30    a 90.1 wt% pure (anhydrous basis) KLG product was recovered corresponding to 51.6% KLG recovery. The composition of the mother liquor is given in Table 2. The combination of additional sulfuric acid and cation exchange led to overprotonation as reflected by the ratio of available protons to KLG in the feed of 133.3% and it became more so as KLG was crystallized as the ratio increased to 239.3% in the mother liquor.

5    Example 27

To simulate mother liquor recycle in a continuous crystallization process, 407.6 grams of the mother liquor from the batch crystallization described in Example 26 was combined with 2959.6 grams of the same fresh feed and subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the average  
10    concentration of soluble inorganics (K, Na, and P) increased by a factor of 9.52 in the mother liquor, or filtrate, relative to that in the fresh feed and 2158.6 grams of distillate was recovered. After vacuum filtration, a methanol wash, and drying, 267.41 grams of a 86.5 wt% pure (anhydrous basis) KLG product was recovered corresponding to 53.5% KLG recovery. The composition of the resultant mother liquor is given in Table  
15    2. Compared to Example 26, the increased concentration factor and addition of even further overprotonated mother liquor to the fresh feed led to a greater surplus of protons as reflected by the ratio of available protons to KLG (377.1% versus 239.3%). Again, there was evidence for KLG decomposition as the mother liquor contained 1.4 wt% ascorbic acid.

20

Example 28

To further simulate mother liquor recycle in a continuous crystallization process, 329.5 grams of the mother liquor from the batch crystallization described in Example 27 was combined with 2519.5 grams of the same fresh feed used in Examples  
25    26 and 27 and subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (K, Na, and P) increased by a factor of 10.32 in the mother liquor, or filtrate, relative to that in the fresh feed and 2053.4 grams of distillate was recovered. After vacuum filtration, a methanol wash, and drying, 247.18 grams of a 86.8 wt% pure (anhydrous basis) KLG  
30    product was recovered corresponding to 60.2% KLG recovery. The composition of the resultant mother liquor is given in Table 2. Again, this mother liquor was overprotonated as reflected by both its ratio of available protons to KLG (395.2%) and ascorbic acid content (2.02 wt%).

5    Example 29

After acidification to pH~2 with sulfuric acid, carbon treatment, and microfiltration to remove cells, carbon and other solids, the same broth used as the fresh feed in Examples 1 and 2 was further pretreated by contact with the hydrogen form of a cation exchange resin. The resultant broth had a composition given in Table 1, of which 3000.2 grams was subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (K, Na, and P) increased by a factor of 5.65 in the mother liquor, or filtrate, relative to that in the feed and 2231.3 grams of distillate was recovered. After vacuum filtration, a methanol wash, and drying, 261.28 grams of a 88.8 wt% pure (anhydrous basis) KLG product was recovered corresponding to 69.4% KLG recovery. The composition of the mother liquor is given in Table 2. The cation exchange led to slight overprotonation as reflected by the ratio of available protons to KLG in the feed of 109.0% and it became more so as KLG was crystallized as the ratio increased to 126.9% in the mother liquor.

20

Example 30

To simulate mother liquor recycle in a continuous crystallization process, 350.3 grams of the mother liquor from the batch crystallization described in Example 29 was combined with 2560 grams of the same fresh feed and subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (K, Na, and P) increased by a factor of 10.03 in the mother liquor, or filtrate, relative to that in the fresh feed and 2167.8 grams of distillate was recovered. After vacuum filtration, a methanol wash, and drying, 294.04 grams of a 88.8 wt% pure (anhydrous basis) KLG product was recovered corresponding to 71.9% KLG recovery. The composition of the resultant mother liquor is given in Table 2. The overprotonated feed and relatively high degree of concentration led to a higher ratio (159.9%) of available protons to KLG in this mother liquor compared to that from Example 29.

30



5    Example 31

To further simulate mother liquor recycle in a continuous crystallization process, 289 grams of the mother liquor from the batch crystallization described in Example 30 was combined with 2522.8 grams of the same fresh feed used in Examples 29 and 30 and subjected to evaporative crystallization at 10°C. The broth was  
10    evaporated to the point at which the average concentration of soluble inorganics (K, Na, and P) increased by a factor of 13.23 in the mother liquor, or filtrate, relative to that in the fresh feed and 2116.5 grams of distillate was recovered. After vacuum filtration, a methanol wash, and drying, 317.18 grams of a 81.1 wt% pure (anhydrous basis) KLG product was recovered corresponding to 76.9% KLG recovery. The composition of the  
15    resultant mother liquor is given in Table 2. Again, this mother liquor was overprotonated as reflected by its ratio of available protons to KLG (177.4%).

Example 32

The same broth used as the fresh feed in Examples 23-25 was further pretreated  
20    by adding more sulfuric acid, filtration, and contact with the hydrogen form of a cation exchange resin much like the fresh feed used in Examples 6, 7 and 26-28. The additional sulfuric acid was intended to fully protonate the KLG and was based upon a C<sup>13</sup> NMR measurement of the degree of proton association with KLG in the broth. The resultant broth had a composition given in Table 1, of which 3100.4 grams was  
25    subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (Na and P) increased by a factor of 5.95 in the mother liquor, or filtrate, relative to that in the feed and 2341 grams of distillate was recovered. After vacuum filtration, a methanol wash, and drying, 246.84 grams of a 88.4 wt% pure (anhydrous basis) KLG product was  
30    recovered corresponding to 61.4% KLG recovery. The composition of the mother liquor is given in Table 2. The combination of additional sulfuric acid and cation exchange led to overprotonation as reflected by the ratio of available protons to KLG in the feed of 133.7% and it became more so as KLG was crystallized as the ratio increased to 242.7% in the mother liquor.

5    Example 33

To simulate mother liquor recycle in a continuous crystallization process, 381.7 grams of the mother liquor from the batch crystallization described in Example 32 was combined with 2663.9 grams of the same fresh feed and subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the average  
10    concentration of soluble inorganics (Na and P) increased by a factor of 10.94 in the mother liquor, or filtrate, relative to that in the fresh feed and 2231.1 grams of distillate was recovered. After vacuum filtration, a methanol wash, and drying, 299.63 grams of a 85.7 wt% pure (anhydrous basis) KLG product was recovered corresponding to 70.0% KLG recovery. The composition of the resultant mother liquor is given in Table  
15    2. Compared to Example 32, the increased concentration factor and addition of even further overprotonated mother liquor to the fresh feed led to a greater surplus of protons as reflected by the ratio of available protons to KLG (448.6% versus 242.7%). Again, there was evidence for KLG decomposition as the mother liquor contained 1.4 wt% ascorbic acid.

20

Example 34

To further simulate mother liquor recycle in a continuous crystallization process, 308.3 grams of the mother liquor from the batch crystallization described in Example 33 was combined with 2600 grams of the same fresh feed used in Examples  
25    32 and 33 and subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (Na and P) increased by a factor of 12.71 in the mother liquor, or filtrate, relative to that in the fresh feed and 2189.9 grams of distillate was recovered. After vacuum filtration, a methanol wash, and drying, 318.36 grams of a 80.5 wt% pure (anhydrous basis) KLG  
30    product was recovered corresponding to 76.4% KLG recovery. The composition of the resultant mother liquor is given in Table 2. Again, this mother liquor was overprotonated as reflected by both its ratio of available protons to KLG (463.1%) and ascorbic acid content (2.65 wt%).

Analysis of the crystallization results from Examples 1-34 shows the impact of  
35    protonation on KLG solubility and decomposition. As shown in Figure 2, KLG

5 solubility decreased as the ratio of available protons to KLG in the mother liquor increased. Given recovery via crystallization improves as the solubility is reduced, these results suggest protonation should be as high as possible in the crystallizer to maximize recovery. However, as shown in Figure 3, KLG decomposition as measured by ascorbic acid content also increased as the ratio of available protons to KLG in the  
10 mother liquor increased. Examples 35-44 reflect initial attempts to moderate the effects of feed protonation on KLG crystallization using anion exchange, careful acidification, and buffering.

#### Example 35

15 After acidification to pH~2 with sulfuric acid, carbon treatment, and microfiltration to remove cells, carbon and other solids, the same broth used as the fresh feed in Examples 1 and 2 was further pretreated by contact with the hydrogen form of a cation exchange resin followed by contact with the hydroxyl form of an anion exchange resin. The resultant broth had a composition given in Table 1, of which  
20 9013.5 grams was subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (Ca, K, Na, and Mg) increased by a factor of 4.01 in the mother liquor, or filtrate, relative to that in the feed and 6497.7 grams of distillate was recovered. After vacuum filtration, two water washes, and drying, 209.30 grams of a 88.2 wt% pure (anhydrous basis)  
25 KLG product was recovered corresponding to 24.7% KLG recovery. The composition of the mother liquor is given in Table 2. While the anion exchange was very effective in removing the inorganic anions (i.e., P, S, and Cl), the cation exchange was incomplete leaving some inorganic cations (i.e., Ca, K, Na, and Mg) in the feed broth. As a result, the pretreated feed was underprotonated as reflected by the ratio of  
30 available protons to KLG in the feed of 95.2% which changed very little upon crystallization (96.9%) due to the relatively low degree of concentration and KLG crystallization.

5    Example 36

To simulate mother liquor recycle in a continuous crystallization process, 2188.3 grams of the mother liquor from the batch crystallization described in Example 35 was subjected to further evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (Ca, K, Na, and Mg) increased by a factor of 16.37 in the mother liquor, or filtrate, relative to that in the fresh feed and 1141.3 grams of distillate was recovered. After vacuum filtration, two water washes, and drying, 499.03 grams of a 78.8 wt% pure (anhydrous basis) KLG product was recovered corresponding to 71.4% KLG recovery. The composition of the resultant mother liquor is given in Table 2. Compared to Example 35, the increased concentration led to a greater deficit of protons as reflected by both the ratio of available protons to KLG (88.5% versus 96.9%) and the mother liquor pH (1.8 versus 1.49). This example illustrates a shortcoming of simply following cation exchange with anion exchange as a means of properly protonating the solution. Unless the ion exchange steps are nearly perfectly performed, the resultant solution may still be improperly protonated.

Example 37

After acidification to pH~2 with sulfuric acid, carbon treatment, and microfiltration to remove cells, carbon and other solids, the same broth used as the fresh feed in Examples 1 and 2 was further pretreated by contact with the hydrogen form of a cation exchange resin followed by contact with the hydroxyl form of an anion exchange resin much like Example 35. The resultant broth had a composition given in Table 1, of which 8999.9 grams was subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (Ca, K, Na, and Mg) increased by a factor of 3.92 in the mother liquor, or filtrate, relative to that in the feed and 6450.1 grams of distillate was recovered. After vacuum filtration, two water washes, and drying, 203.59 grams of a 86.8 wt% pure (anhydrous basis) KLG product was recovered corresponding to 23.4% KLG recovery. The composition of the mother liquor is given in Table 2. Again, while the anion exchange was very effective in removing the inorganic anions (i.e., P, S, and Cl), the

5 cation exchange was incomplete leaving some inorganic cations (i.e., Ca, K, Na, and Mg) in the feed broth. As a result, the pretreated feed was underprotonated as reflected by the ratio of available protons to KLG in the feed of 95.3% which changed very little upon crystallization (97.1%) due to the relatively low degree of concentration and KLG crystallization.

10

#### Example 38

To simulate mother liquor recycle in a continuous crystallization process, 2211.4 grams of the mother liquor from the batch crystallization described in Example 37 was subjected to further evaporative crystallization at 10°C. The broth was  
15 evaporated to the point at which the average concentration of soluble inorganics (Ca, K, Na, and Mg) increased by a factor of 16.57 in the mother liquor, or filtrate, relative to that in the fresh feed and 1161.6 grams of distillate was recovered. After vacuum filtration, two water washes, and drying, 485.3 grams of a 78.8 wt% pure (anhydrous basis) KLG product was recovered corresponding to 72.6% KLG recovery. The  
20 composition of the resultant mother liquor is given in Table 2. Compared to Example 37, the increased concentration led to a greater deficit of protons as reflected by both the ratio of available protons to KLG (89.0% versus 97.1%) and the mother liquor pH (1.83 versus 1.5). Again, this example illustrates a shortcoming of simply following cation exchange with anion exchange as a means of properly protonating the solution.

25

#### Example 39

After acidification to pH~2 with sulfuric acid, carbon treatment, and microfiltration to remove cells, carbon and other solids, the same broth used as the fresh feed in Examples 1 and 2 was further pretreated by adding more sulfuric acid and  
30 filtration much like Example 17. The additional sulfuric acid was that required to fully protonate the KLG based upon a  $C^{13}$  NMR measurement of the degree of proton association with KLG in the broth. The resultant broth had a composition given in Table 1, of which 9001.6 grams was subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble  
35 inorganics (K, Na, Mg, P, and Cl) increased by a factor of 5.05 in the mother liquor, or

5 filtrate, relative to that in the feed and 6391.8 grams of distillate was recovered. After vacuum filtration, two water washes, and drying, 797.4 grams of a 79.6 wt% pure (anhydrous basis) KLG product was recovered corresponding to 58.4% KLG recovery. The composition of the mother liquor is given in Table 2. The additional sulfuric acid alone led to overprotonation as reflected by the ratio of available protons to KLG in the  
10 feed of 111.4% and it became more so as KLG was crystallized as the ratio increased to 130.5% in the mother liquor.

#### Example 40

To simulate mother liquor recycle in a continuous crystallization process, 1226  
15 grams of the mother liquor from the batch crystallization described in Example 39 was subjected to further evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (K, Na, Mg, P, and Cl) increased by a factor of 12.17 in the mother liquor, or filtrate, relative to that in the fresh feed and 491.7 grams of distillate was recovered. After vacuum filtration, two  
20 water washes, and drying, 232.2 grams of a 70.4 wt% pure (anhydrous basis) KLG product was recovered corresponding to 57.6% KLG recovery. The composition of the resultant mother liquor is given in Table 2. Compared to Example 39, the increased concentration led to a greater surplus of protons as reflected by both the ratio of available protons to KLG (199.1% versus 130.5%) and the mother liquor pH (0.46  
25 versus 0.91). There was also evidence for KLG decomposition as the ascorbic acid level in the mother liquor was 2.41 wt%.

#### Example 41

After acidification to pH~2 with sulfuric acid, carbon treatment, and  
30 microfiltration to remove cells, carbon and other solids, the same broth used as the fresh feed in Examples 1 and 2 was further pretreated by adding more sulfuric acid and filtration much like Examples 17 and 39. The additional sulfuric acid was that required to fully protonate the KLG based upon a C<sup>13</sup> NMR measurement of the degree of proton association with KLG in the broth. The resultant broth had a composition given  
35 in Table 1, of which 9000 grams was subjected to evaporative crystallization at 10°C.

- 5 The broth was evaporated to the point at which the average concentration of soluble inorganics (K, Na, Mg, P, and Cl) increased by a factor of 4.76 in the mother liquor, or filtrate, relative to that in the feed and 6346.1 grams of distillate was recovered. After vacuum filtration, two water washes, and drying, 767.1 grams of a 87.8 wt% pure (anhydrous basis) KLG product was recovered corresponding to 62.2% KLG recovery.
- 10 The composition of the mother liquor is given in Table 2. The additional sulfuric acid alone led to overprotonation as reflected by the ratio of available protons to KLG in the feed of 110.2% and it became more so as KLG was crystallized as the ratio increased to 127.3% in the mother liquor.

15 Example 42

- To simulate mother liquor recycle in a continuous crystallization process, 1458.4 grams of the mother liquor from the batch crystallization described in Example 41 was subjected to further evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (K, Na, Mg, P, and Cl) increased by a factor of 12.13 in the mother liquor, or filtrate, relative to that in the fresh feed and 671.0 grams of distillate was recovered. After vacuum filtration, two water washes, and drying, 293.4 grams of a 73.0 wt% pure (anhydrous basis) KLG product was recovered corresponding to 65.7% KLG recovery.
- 20 The composition of the resultant mother liquor is given in Table 2. Compared to Example 41, the increased concentration led to a greater surplus of protons as reflected by both the ratio of available protons to KLG (193.5% versus 127.3%) and the mother liquor pH (0.71 versus 1.05). There was also evidence for KLG decomposition as the ascorbic acid level in the mother liquor was 1.82 wt%.

30 Example 43

- The same broth used as the fresh feed in Examples 23-25 was further pretreated by contact with the hydrogen form of a cation exchange resin much like the fresh feed used in Examples 14-16. Sodium sulfate salt was subsequently added to the broth in an attempt to moderate the increasing proton concentration upon evaporation. The resultant broth had a composition given in Table 1, of which 9000.2 grams was
- 35

5 subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (Na and P) increased by a factor of 6.21 in the mother liquor, or filtrate, relative to that in the feed and 6858.7 grams of distillate was recovered. After vacuum filtration, two water washes, and drying, 720.1 grams of a 86.6 wt% pure (anhydrous basis) KLG product was recovered  
10 corresponding to 67.4% KLG recovery. The composition of the mother liquor is given in Table 2. Sodium sulfate addition was ineffective in reducing the overprotonation resulting from cation exchange as the ratio of available protons to KLG in the feed was 110.1% and increased to 134.8% in the mother liquor while the pH decreased from 1.55 to 0.65.

15

#### Example 44

To simulate mother liquor recycle in a continuous crystallization process, 1110.7 grams of the mother liquor from the batch crystallization described in Example 43 was subjected to further evaporative crystallization at 10°C. The broth was  
20 evaporated to the point at which the average concentration of soluble inorganics (Na and P) increased by a factor of 14.24 in the mother liquor, or filtrate, relative to that in the fresh feed and 450.3 grams of distillate was recovered. After vacuum filtration, two water washes, and drying, 182.4 grams of a 74.8 wt% pure (anhydrous basis) KLG product was recovered corresponding to 63.1% KLG recovery. The composition of the  
25 resultant mother liquor is given in Table 2. Compared to Example 43, the increased concentration led to a greater surplus of protons as reflected by the ratio of available protons to KLG (202.5% versus 134.8%). There was also evidence for KLG decomposition as the ascorbic acid level in the mother liquor was 1.57 wt%.

In all of these cases (Examples 1-44), no attempt was made to adjust the  
30 protonation level of the pretreated broth based on charge balance calculations or titrations. As a result, the crystallization feeds were either under- or overacidified leading to high KLG solubilities or KLG decomposition, respectively, upon concentration by evaporation. In the following examples, KLG protonation was adjusted in a final base or acid addition step before crystallization such that the molar  
35 ratio of available protons to KLG was targeted to be one (i.e., equivalence).



5    Example 45

          The same broth used as the fresh feed in Examples 23-25 was further pretreated by contact with the hydrogen form of a cation exchange resin much like the fresh feed used in Examples 14-16. Three separate batches were prepared (designated 45A, 45B, and 45C) with compositions given in Table 3. Based on charge balance calculations, sodium hydroxide (2.4 grams/kg broth) was added to the blended broth to bring the ratio of available protons to KLG near 100%. The resultant broth had a composition given in Table 1, of which 9000 grams was subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (Na and P) increased by a factor of 6.69 in the mother liquor, or filtrate, relative to that in the feed and 6869.2 grams of distillate was recovered. After vacuum filtration, two water washes, and drying, 700.4 grams of a 84.1 wt% pure (anhydrous basis) KLG product was recovered corresponding to 63.2% KLG recovery. The composition of the mother liquor is given in Table 2. Sodium hydroxide addition was very effective in reducing the overprotonation resulting from cation exchange as the ratio of available protons to KLG in the feed was 101.9% and increased to only 105.7% in the mother liquor.

Example 46

          To simulate mother liquor recycle in a continuous crystallization process, 1109.8 grams of the mother liquor from the batch crystallization described in Example 45 was subjected to further evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (Na and P) increased by a factor of 14.77 in the mother liquor, or filtrate, relative to that in the fresh feed and 451.7 grams of distillate was recovered. After vacuum filtration, two water washes, and drying, 148.6 grams of a 82.9 wt% pure (anhydrous basis) KLG product was recovered corresponding to 51.7% KLG recovery. The composition of the resultant mother liquor is given in Table 2. Consistent with the increased concentration and KLG precipitation, there was a slightly greater surplus of protons as reflected by the ratio of available protons to KLG in the mother liquor (113.5% versus 105.7% in Example 45). However, this degree of overacidification was quite modest relative to

5 that observed at similar concentration levels in Example 44 where sodium sulfate was added to the same cation exchanged broth instead of sodium hydroxide. The degree of KLG decomposition was reduced as ascorbic acid levels in the mother liquor were only 0.88 wt% in this case compared to 1.57 wt% in Example 44.

10 Example 47

As suggested by the nearly identical compositions in Table 1, 9000.4 grams of the same broth used as the fresh feed in Example 45 was again subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (Na and P) increased by a factor of 6.48 in the  
15 mother liquor, or filtrate, relative to that in the feed and 6902.4 grams of distillate was recovered. After vacuum filtration, two water washes, and drying, 708.5 grams of a 85.9 wt% pure (anhydrous basis) KLG product was recovered corresponding to 65.2% KLG recovery. The composition of the mother liquor is given in Table 2. Again, sodium hydroxide addition was very effective in reducing the overprotonation resulting  
20 from cation exchange as the ratio of available protons to KLG in the feed was 102.1% and increased to only 105.6% in the mother liquor.

Example 48

To simulate mother liquor recycle in a continuous crystallization process,  
25 1117.8 grams of the mother liquor from the batch crystallization described in Example 47 was subjected to further evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (Na and P) increased by a factor of 15.24 in the mother liquor, or filtrate, relative to that in the fresh feed and 452.3 grams of distillate was recovered. After vacuum filtration, two  
30 water washes, and drying, 248.8 grams of a 70.4 wt% pure (anhydrous basis) KLG product was recovered corresponding to 70.9% KLG recovery. The composition of the resultant mother liquor is given in Table 2. Consistent with the increased concentration and KLG precipitation relative to Example 46, there was a slightly greater surplus of protons as reflected by the ratio of available protons to KLG in the mother liquor  
35 (117.7% versus 113.5%). Again, however, this degree of overacidification was quite

5 modest relative to that observed in Example 44 where sodium sulfate was added to the same cation exchanged broth instead of sodium hydroxide. The degree of KLG decomposition was again low, as the ascorbic acid level in the mother liquor was only 0.89 wt%.

10 Example 49

After acidification to pH~2 with sulfuric acid, carbon treatment, and microfiltration to remove cells, carbon, and other solids, a broth was further pretreated by contact with the hydrogen form of a cation exchange resin. Two separate batches were prepared (designated 49A and 49B) with compositions given in Table 3. A one-  
15 ml sample of each was transferred to a 100-ml titration vessel and mixed with 0.2 ml of a 1M barium chloride solution. (This amount of barium chloride was in excess relative to the sulfate present in the sample.) To each solution was added 75 ml of dimethyl sulfoxide (DMSO) and 0.3 ml of 0.5M sodium hydroxide. Each solution was then titrated to equivalence with a 0.1M solution of sodium triflic acid in DMSO. By  
20 titration, 0.0445 and 0.0326 moles of base per kg of broth were needed to bring solutions 49A and 49B, respectively, to equivalence.

Charge balance calculations were also performed for these broths. By charge balance, 0.0445 and 0.0324 moles of base per kg of broth were needed to bring solutions 49A and 49B, respectively, to equivalence thereby establishing either method  
25 as a valid means to measure the state of protonation.

After addition of 1.78 and 1.31 grams of NaOH per kg of broths 49A and 49B, respectively, to bring them to equivalence, the broths were blended together. The resultant broth had a composition given in Table 1, of which 6500.1 grams was subjected to evaporative crystallization at 10°C. The broth was evaporated to the point  
30 at which the average concentration of soluble inorganics (Na, Mg, and P) increased by a factor of 5.36 in the mother liquor, or filtrate, relative to that in the feed and 4596.7 grams of distillate was recovered. After vacuum filtration, two water washes, and drying, 695.5 grams of a 90.4 wt% pure (anhydrous basis) KLG product was recovered corresponding to 69.6% KLG recovery. The composition of the mother liquor is given  
35 in Table 2. Again, sodium hydroxide addition was very effective in reducing the

5 overprotonation resulting from cation exchange as the ratio of available protons to KLG in the feed was 100.7% and increased to only 101.4% in the mother liquor. This was also reflected by the modest decrease in pH from 1.36 in the feed to 1.18 in the mother liquor.

10 Example 50

To simulate mother liquor recycle in a continuous crystallization process, 894.7 grams of the mother liquor from the batch crystallization described in Example 49 was subjected to further evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (Na, Mg, and P)  
15 increased by a factor of 16.07 in the mother liquor, or filtrate, relative to that in the fresh feed and 396.6 grams of distillate was recovered. After vacuum filtration, two water washes, and drying, 194.5 grams of a 77.0 wt% pure (anhydrous basis) KLG product was recovered corresponding to 62.5% KLG recovery. The composition of the resultant mother liquor is given in Table 2. Consistent with the increased concentration  
20 and KLG precipitation relative to Example 49, there was a slightly greater surplus of protons as reflected by the ratio of available protons to KLG in the mother liquor (105.3% versus 101.4%). Again, however, this degree of overacidification was quite modest as the pH of the second-stage mother liquor dropped to only 1.13.

25 Example 51

As suggested by the nearly identical compositions in Table 1, 6500.5 grams of the same broth used as the fresh feed in Example 49 was again subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (Na, Mg, and P) increased by a factor of 5.31 in the  
30 mother liquor, or filtrate, relative to that in the feed and 4612.1 grams of distillate was recovered. After vacuum filtration, two water washes, and drying, 683.7 grams of a 84.7 wt% pure (anhydrous basis) KLG product was recovered corresponding to 65.8% KLG recovery. The composition of the mother liquor is given in Table 2. Again, sodium hydroxide addition was very effective in reducing the overprotonation resulting  
35 from cation exchange as the ratio of available protons to KLG in the feed was 100.6%

- 5 and increased to only 101.6% in the mother liquor. This was also reflected by the modest decrease in pH from 1.33 in the feed to 1.21 in the mother liquor.

#### Example 52

- To simulate mother liquor recycle in a continuous crystallization process,  
10 1045.9 grams of the mother liquor from the batch crystallization described in Example 51 was subjected to further evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (Na, Mg, and P) increased by a factor of 13.79 in the mother liquor, or filtrate, relative to that in the fresh feed and 439.6 grams of distillate was recovered. After vacuum  
15 filtration, two water washes, and drying, 192.6 grams of a 85.9 wt% pure (anhydrous basis) KLG product was recovered corresponding to 63.0% KLG recovery. The composition of the resultant mother liquor is given in Table 2. Consistent with the increased concentration and KLG precipitation relative to Example 51, there was a slightly greater surplus of protons as reflected by the ratio of available protons to KLG  
20 in the mother liquor (104.0% versus 101.6%). Again, however, this degree of overacidification was quite modest, as the pH of the second-stage mother liquor dropped to only 1.18 and ascorbic acid content was only 1.02 wt%.

#### Example 53

- 25 After acidification to pH~2 with sulfuric acid, carbon treatment, and microfiltration to remove cells, carbon, and other solids, a broth was further pretreated by contact with the hydrogen form of a cation exchange resin. A portion of this cation-exchanged broth was further pretreated by contact with the hydroxyl form of an anion exchange resin. To simulate a continuous crystallization process with cation exchange  
30 of the fresh feed and anion exchange of the recycled mother liquor, some of the cation-exchanged only broth was combined with the cation- and anion-exchanged broth and sodium hydroxide such that the combined feed was near equivalence. The resultant broth had a composition given in Table 1, of which 9002.4 grams was subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the  
35 average concentration of soluble inorganics (Na, S, and P) increased by a factor of 7.65

5 in the mother liquor, or filtrate, relative to that in the feed and 7131.8 grams of distillate was recovered. After vacuum filtration, two water washes, and drying, 652.4 grams of a 87.0 wt% pure (anhydrous basis) KLG product was recovered corresponding to 67.5% KLG recovery. The composition of the mother liquor is given in Table 2. The combination of partial anion exchange and sodium hydroxide addition was effective in  
10 reducing the overprotonation resulting from cation exchange as the ratio of available protons to KLG in the feed was 102.0% and increased to only 106.7% in the mother liquor.

#### Example 54

15 To further simulate mother liquor recycle and increased recovery from increasing concentrations, 971.6 grams of the mother liquor from the batch crystallization described in Example 53 was subjected to further evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (Na, S, and P) increased by a factor of 19.92 in the  
20 mother liquor, or filtrate, relative to that in the fresh feed and 466.9 grams of distillate was recovered. After vacuum filtration, two water washes, and drying, 147.4 grams of a 81.8 wt% pure (anhydrous basis) KLG product was recovered corresponding to 53.5% KLG recovery. The composition of the resultant mother liquor is given in Table 2. Consistent with the increased concentration and KLG precipitation relative to  
25 Example 53, there was a greater surplus of protons as reflected by the ratio of available protons to KLG in the mother liquor (119.7% versus 106.7%). Even at nearly 20-fold concentration, this degree of overacidification was modest, as the pH of the second-stage mother liquor dropped to only 0.63 and ascorbic acid content was only 1.51 wt%.

#### Example 55

30 As suggested by the nearly identical compositions in Table 1, 9000.1 grams of the same broth used as the fresh feed in Example 53 was again subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (Na, S, and P) increased by a factor of 7.30 in the  
35 mother liquor, or filtrate, relative to that in the feed and 7118.2 grams of distillate was

5 recovered. After vacuum filtration, two water washes, and drying, 647.6 grams of a  
89.2 wt% pure (anhydrous basis) KLG product was recovered corresponding to 69.1%  
KLG recovery. The composition of the mother liquor is given in Table 2. Again, the  
combination of partial anion exchange and sodium hydroxide addition was effective in  
reducing the overprotonation resulting from cation exchange as the ratio of available  
10 protons to KLG in the feed was 102.1% and increased to only 105.9% in the mother  
liquor.

#### Example 56

To further simulate mother liquor recycle and increased recovery from  
15 increasing concentrations, 997.3 grams of the mother liquor from the batch  
crystallization described in Example 55 was subjected to further evaporative  
crystallization at 10°C. The broth was evaporated to the point at which the average  
concentration of soluble inorganics (Na, S, and P) increased by a factor of 16.85 in the  
mother liquor, or filtrate, relative to that in the fresh feed and 514.8 grams of distillate  
20 was recovered. After vacuum filtration, two water washes, and drying, 156.4 grams of  
a 84.5 wt% pure (anhydrous basis) KLG product was recovered corresponding to  
57.3% KLG recovery. The composition of the resultant mother liquor is given in Table  
2. Consistent with the increased concentration and KLG precipitation relative to  
Example 55, there was a greater surplus of protons as reflected by the ratio of available  
25 protons to KLG in the mother liquor (115.2% versus 105.9%). The slightly higher pH  
of the second-stage mother liquor (0.66 versus 0.63) and lower ascorbic acid level (1.27  
versus 1.51 wt%) relative to Example 54 likely reflect the smaller degree of  
concentration.

#### 30 Example 57

After microfiltration at pH~5.5 to remove cells, acidification to pH~2.3 with  
sulfuric acid, carbon treatment, and filtration to remove carbon and other solids, a broth  
was further pretreated by adding more sulfuric acid (to pH 1.8), filtration, and contact  
with the hydrogen form of a cation exchange resin. Based on charge balance  
35 calculations using the pretreated broth composition in Table 3, sodium hydroxide (2.94

5 grams/kg broth) was added to the blended broth to bring it near equivalence. The resultant broth had a composition given in Table 1, of which 9000 grams was subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (K, Na, Mg, Cl, and P) increased by a factor of 7.63 in the mother liquor, or filtrate, relative to that in the feed and 6972.9  
10 grams of distillate was recovered. After vacuum filtration, two water washes, and drying, 869.3 grams of a 87.9 wt% pure (anhydrous basis) KLG product was recovered corresponding to 76.5% KLG recovery. The composition of the mother liquor is given in Table 2. Sodium hydroxide addition was very effective in reducing the overprotonation resulting from cation exchange as the ratio of available protons to KLG  
15 in the feed was 99.6% and increased to only 100.8% in the mother liquor. This was also reflected by the small decrease in pH from 1.52 to 1.25 and the low level of ascorbic acid generated (0.34 wt%).

#### Example 58

20 As suggested by the nearly identical compositions in Table 1, 9000.4 grams of the same broth used as the fresh feed in Example 57 was again subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (K, Na, Mg, Cl, and P) increased by a factor of 7.37 in the mother liquor, or filtrate, relative to that in the feed and 6955.5 grams of distillate  
25 was recovered. After vacuum filtration, two water washes, and drying, 838.6 grams of a 82.7 wt% pure (anhydrous basis) KLG product was recovered corresponding to 64.6% KLG recovery. The composition of the mother liquor is given in Table 2. Again, sodium hydroxide addition was very effective in reducing the overprotonation resulting from cation exchange as the ratio of available protons to KLG in the feed was  
30 100.6% and increased to only 101.6% in the mother liquor. This was also reflected by the small decrease in pH from 1.52 in the feed to 1.3 in the mother liquor and the low ascorbic acid level of 0.37 wt%.



5     Example 59

After microfiltration at pH~5.5 to remove cells, acidification to pH~2.3 with sulfuric acid, carbon treatment, and filtration to remove carbon and other solids, a broth was further pretreated by adding more sulfuric acid (to pH 1.8), filtration, and contact with the hydrogen form of a cation exchange resin. A portion of this cation-exchanged  
10     broth was further pretreated by contact with the hydroxyl form of an anion exchange resin. To simulate a continuous crystallization process with cation exchange of the fresh feed and anion exchange of the recycled mother liquor, some of the cation-exchanged only broth was combined with the cation- and anion-exchanged broth and both sodium hydroxide and sulfuric acid such that the combined feed was near  
15     equivalence. The resultant broth had a composition given in Table 1, of which 9000.4 grams was subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (K, Na, Mg, Cl, and P) increased by a factor of 6.96 in the mother liquor, or filtrate, relative to that in the feed and 7001 grams of distillate was recovered. After vacuum filtration, two water  
20     washes, and drying, 720.2 grams of a 86.3 wt% pure (anhydrous basis) KLG product was recovered corresponding to 64.0% KLG recovery. The composition of the mother liquor is given in Table 2. The combination of partial anion exchange and sodium hydroxide addition was effective in reducing the overprotonation resulting from cation exchange as the ratio of available protons to KLG in the feed was 100.8% and  
25     increased to only 103.0% in the mother liquor. This was also reflected by the small decrease in pH from 1.51 in the feed to 1.34 in the mother liquor and the low ascorbic acid level of 0.40 wt%.

Example 60

30     As suggested by the nearly identical compositions in Table 1, 9000.1 grams of the same broth used as the fresh feed in Example 59 was again subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (K, Na, Mg, Cl, and P) increased by a factor of 7.05 in the mother liquor, or filtrate, relative to that in the feed and 7001.2 grams of distillate  
35     was recovered. After vacuum filtration, two water washes, and drying, 700.8 grams of

5 a 87.1 wt% pure (anhydrous basis) KLG product was recovered corresponding to 67.6% KLG recovery. The composition of the mother liquor is given in Table 2. Again, the combination of partial anion exchange and sodium hydroxide addition was effective in reducing the overprotonation resulting from cation exchange as the ratio of available protons to KLG in the feed was 101.0% and increased to only 102.9% in the  
10 mother liquor. And, KLG decomposition was minimal as indicated by the low ascorbic acid level of 0.44 wt% in the mother liquor.

#### Example 61

After microfiltration at pH~5.5 to remove cells, acidification to pH~2 with  
15 sulfuric acid, carbon treatment, and filtration to remove carbon and other solids, a broth was further pretreated by contact with the hydrogen form of a cation exchange resin. A portion of this cation-exchanged broth was further pretreated by contact with the hydroxyl form of an anion exchange resin. To simulate a continuous crystallization process with cation exchange of the fresh feed and anion exchange of the recycled  
20 mother liquor, some of the cation-exchanged only broth was combined with the cation- and anion-exchanged broth such that the composite feed was near equivalence. The resultant broth had a composition given in Table 1, of which 9000.1 grams was subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (K, Na, Mg, and P) increased  
25 by a factor of 9.82 in the mother liquor, or filtrate, relative to that in the feed and 7412.7 grams of distillate was recovered. After vacuum filtration, two water washes, and drying, 671.1 grams of a 85.5 wt% pure (anhydrous basis) KLG product was recovered corresponding to 70.3% KLG recovery. The composition of the mother liquor is given in Table 2. Because the cation exchange was relatively incomplete, the  
30 feed was somewhat underprotonated as reflected by the ratio of available protons to KLG of 97.7% and become slightly more so (93.5%) in the resulting mother liquor.

#### Example 62

As suggested by the nearly identical compositions in Table 1, 9000.7 grams of  
35 the same broth used as the fresh feed in Example 61 was again subjected to evaporative

5 crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (K, Na, Mg, Cl, and P) increased by a factor of 9.26 in the mother liquor, or filtrate, relative to that in the feed and 7366.2 grams of distillate was recovered. After vacuum filtration, two water washes, and drying, 630.1 grams of a 87.9 wt% pure (anhydrous basis) KLG product was recovered corresponding to  
10 74.9% KLG recovery. The composition of the mother liquor is given in Table 2. Again, because the cation exchange was relatively incomplete, the feed was somewhat underprotonated as reflected by the ratio of available protons to KLG of 97.4% and become slightly more so (93.5%) in the resulting mother liquor. KLG decomposition was minimal as indicated by the low ascorbic acid level of 0.37 wt% in the mother  
15 liquor.

### Example 63

After microfiltration at pH~5.5 to remove cells, acidification to pH~2 with sulfuric acid, and filtration to remove solids, a broth was further pretreated by contact  
20 with the hydrogen form of a cation exchange resin. Based on charge balance calculations using the pretreated broth composition in Table 3, sodium hydroxide (7.5 grams/kg broth) was added to the blended broth to bring it near equivalence. The resultant broth had a composition given in Table 1, of which 8999.5 grams was subjected to evaporative crystallization at 10°C. The broth was evaporated to the point  
25 at which the average concentration of soluble inorganics (Na, Mg, Cl, and P) increased by a factor of 7.12 in the mother liquor, or filtrate, relative to that in the feed and 6541.2 grams of distillate was recovered. After vacuum filtration, two water washes, and drying, 975.7 grams of a 80.6 wt% pure (anhydrous basis) KLG product was recovered corresponding to 72.3% KLG recovery. The composition of the mother  
30 liquor is given in Table 2. Sodium hydroxide addition was effective in reducing the overprotonation resulting from cation exchange as the ratio of available protons to KLG in the feed was 102.3% and increased to only 106.2% in the mother liquor. KLG decomposition was minimal as indicated by the low ascorbic acid level of 0.60 wt% in the mother liquor.

5    Example 64

To simulate mother liquor recycle in a continuous crystallization process, 921.5 grams of the mother liquor from the batch crystallization described in Example 63 was subjected to further evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (Na, Mg, Cl, and P) increased by a factor of 8.74 in the mother liquor, or filtrate, relative to that in the fresh feed and 232.2 grams of distillate was recovered. After vacuum filtration, two water washes, and drying, 73.3 grams of a 76.0 wt% pure (anhydrous basis) KLG product was recovered corresponding to 27.5% KLG recovery. The composition of the resultant mother liquor is given in Table 2. Consistent with the increased concentration and KLG precipitation relative to Example 63, there was a greater surplus of protons as reflected by the ratio of available protons to KLG in the mother liquor (116.0% versus 106.2%). Again, however, this degree of overacidification was quite modest, as the ascorbic acid content of the second-stage mother liquor was only 0.94 wt%.

20    Example 65

After microfiltration at pH~5.5 to remove cells, acidification to pH~2 with sulfuric acid, carbon treatment, and filtration to remove carbon and other solids, a broth was further pretreated by contact with the hydrogen form of a cation exchange resin. A portion of this cation-exchanged broth was further pretreated by contact with the hydroxyl form of an anion exchange resin. To simulate a continuous crystallization process with cation exchange of the fresh feed and anion exchange of the recycled mother liquor, some of the cation-exchanged only broth was combined with the cation- and anion-exchanged broth and sodium hydroxide such that the composite feed was near equivalence. The resultant broth had a composition given in Table 1, of which 9000.1 grams was subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (S, Cl, and P) increased by a factor of 6.05 in the mother liquor, or filtrate, relative to that in the feed and 6717.2 grams of distillate was recovered. After vacuum filtration, two water washes, and drying, 655 grams of a 85.7 wt% pure (anhydrous basis) KLG product was recovered corresponding to 55.4% KLG recovery. The composition of the

5 mother liquor is given in Table 2. The combination of partial anion exchange and sodium hydroxide addition was effective in reducing the overprotonation resulting from cation exchange as the ratio of available protons to KLG in the feed was 100.4% and increased to only 101.7% in the mother liquor. KLG decomposition was also low as reflected by the ascorbic acid level of 0.41 wt% in the mother liquor.

10

#### Example 66

To further simulate mother liquor recycle and increased recovery from increasing concentrations, 934.2 grams of the mother liquor from the batch crystallization described in Example 65 was subjected to further evaporative  
15 crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (S, Cl, and P) increased by a factor of 27.02 in the mother liquor, or filtrate, relative to that in the fresh feed and 476.8 grams of distillate was recovered. After vacuum filtration, two water washes, and drying, 194.2 grams of a 79.3 wt% pure (anhydrous basis) KLG product was recovered corresponding to  
20 66.7% KLG recovery. The composition of the resultant mother liquor is given in Table 2. Even at nearly 30-fold concentration, the mother liquor remained near equivalence as the ratio of available protons to KLG increased to only 108.1%.

#### Example 67

25 After microfiltration at pH~5.5 to remove cells, acidification to pH~2 with sulfuric acid, and filtration to remove solids, a broth was further pretreated by contact with the hydrogen form of a cation exchange resin. A portion of this cation-exchanged broth was further pretreated by contact with the hydroxyl form of an anion exchange resin. To simulate a continuous crystallization process with cation exchange of the  
30 fresh feed and anion exchange of the recycled mother liquor, some of the cation-exchanged only broth was combined with the cation- and anion-exchanged broth and sodium hydroxide such that the composite feed was near equivalence. The resultant broth had a composition given in Table 1, of which 9000.2 grams was subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the  
35 average concentration of soluble inorganics (Na, S, Cl, and P) increased by a factor of

5 6.87 in the mother liquor, or filtrate, relative to that in the feed and 6925 grams of  
distillate was recovered. After vacuum filtration, two water washes, and drying, 689.7  
grams of a 85.6 wt% pure (anhydrous basis) KLG product was recovered  
corresponding to 58.9% KLG recovery. The composition of the mother liquor is given  
in Table 2. Again, the combination of partial anion exchange and sodium hydroxide  
10 addition was effective in reducing the overprotonation resulting from cation exchange  
as the ratio of available protons to KLG in the feed was 100.3% and increased to only  
101.8% in the mother liquor.

#### Example 68

15 To further simulate mother liquor recycle and increased recovery from  
increasing concentrations, 1054.9 grams of the mother liquor from the batch  
crystallization described in Example 67 was subjected to further evaporative  
crystallization at 10°C. The broth was evaporated to the point at which the average  
concentration of soluble inorganics (Na, S, Cl, and P) increased by a factor of 16.33 in  
20 the mother liquor, or filtrate, relative to that in the fresh feed and 522.3 grams of  
distillate was recovered. After vacuum filtration, two water washes, and drying, 177.3  
grams of a 74.3 wt% pure (anhydrous basis) KLG product was recovered  
corresponding to 51.1% KLG recovery. The composition of the resultant mother liquor  
is given in Table 2. Again, the combination of partial anion exchange and sodium  
25 hydroxide addition was effective in reducing the overprotonation resulting from cation  
exchange as the ratio of available protons to KLG increased to only 106.2% in the  
second-stage mother liquor.

#### Example 69

30 After microfiltration at pH~5.5 to remove cells, acidification to pH~2 with  
sulfuric acid, carbon treatment, and microfiltration to remove cells, carbon and other  
solids, a broth was further pretreated by adding more sulfuric acid and filtration. Based  
on charge balance calculations using the pretreated broth composition in Table 3, the  
additional sulfuric acid (5.31 grams/kg of broth) was that required to bring the solution  
35 near equivalence. The resultant broth had a composition given in Table 1, of which

5 9000 grams was subjected to evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (K, Na, Mg, Cl, and P) increased by a factor of 4.89 in the mother liquor, or filtrate, relative to that in the feed and 6236.4 grams of distillate was recovered. After vacuum filtration, two water washes, and drying, 861.6 grams of a 83.5 wt% pure (anhydrous basis) KLG product was recovered corresponding to 60.0% KLG recovery. The composition of the mother liquor is given in Table 2. Apparently the amount of sulfuric acid added was insufficient to reach equivalence as the feed was somewhat underprotonated as reflected by the ratio of available protons to KLG of 97.0%, and become slightly more so (94.0%) in the resulting mother liquor.

15

#### Example 70

To simulate mother liquor recycle in a continuous crystallization process, 1434.4 grams of the mother liquor from the batch crystallization described in Example 69 was subjected to further evaporative crystallization at 10°C. The broth was evaporated to the point at which the average concentration of soluble inorganics (K, Na, Mg, Cl, and P) increased by a factor of 11.63 in the mother liquor, or filtrate, relative to that in the fresh feed and 664.6 grams of distillate was recovered. After vacuum filtration, two water washes, and drying, 257.4 grams of a 82.1 wt% pure (anhydrous basis) KLG product was recovered corresponding to 56.4% KLG recovery. The composition of the resultant mother liquor is given in Table 2. Consistent with the increased concentration and KLG precipitation relative to Example 63, there was a greater deficit of protons as reflected by the ratio of available protons to KLG in the mother liquor (88.24% versus 94.0%). Again, however, this degree of underacidification was quite modest. And the ascorbic acid content of the second-stage mother liquor of only 0.82 wt% demonstrates that ion exchange is not necessary to avoid KLG decomposition.

30

5

Table 1  
Compositional Analyses and Charge Balance Calculations for Crystallization Feeds

Example	KLG wt%	Ca	K	Na	Ppm Mg	P	S	Cl*	Implied, ppm H <sub>2</sub> O <sup>+</sup>	OH <sup>-</sup>	Protons/KLG,% Total	Avail.
1	13.25	1660	1670	880	0	540	880	221.4	0	857	92.6	87.5
3	12.00	0	0	0	0	510	835	209.1	2043	0	117.4	112.1
6	8.90	2.8	0	11.7	0.58	174	2482	287.1	3407	0	139.1	136.6
8	10.89	0	0	7	0	123	3789	203.0	4827	0	145.2	143.8
11	12.27	0	0	7.83	0	488.5	3849	200.3	5569	0	146.3	141.3
14	8.31	0	0	10.6	0	92.5	762.3	152.6	1148	0	114.1	112.7
17	13.23	637	1700	822	157	508	2796	208.3	2009	0	115.5	110.7
20	12.35	695	1100	778	151	126	2605	207.9	1361	0	111.3	110.0
23	12.12	1050	1580	832	152	131	1035	216.2	0	989	90.7	89.3
26	12.28	18	56	200	4	126	3400	207.9	4163	0	134.6	133.3
29	11.14	15	143	372	6	508	806	208.3	1603	0	114.7	109.0
32	11.46	5	0	99.8	0.8	129	3100	212.9	3943	0	135.1	133.7
35	8.30	41	173	288.1	31.7	9	1.8	30	0	336	95.4	95.2
37	8.38	41	168	292	31.3	6	8.2	26	0	337	95.4	95.3
39	12.07	885	1700	900.8	158	529	3000	218	1993	0	116.9	111.4
41	12.03	529	1700	912	160	536	2600	233	1864	0	115.8	110.2
43	10.29	2	32	1400	0.7	121	1700	199.7	1171	0	111.6	110.1
45	10.36	3	32	1400	0.9	122	1000	201.3	342	0	103.4	101.9
47	10.37	5	36	1400	0.9	125	1000	252	370	0	103.7	102.1
49	13.89	101	53	1000	9.9	180	645.8	345.6	319	0	102.3	100.7
51	13.55	102	58	1000	9.9	177	637	334	293	0	102.2	100.6
53	9.34	0	0	248.1	0	140	230	57.4	356	0	103.9	102.0
55	9.29	0	0	248	0.9	142	224	78	363	0	104.0	102.1
57	11.09	253	177	2000	26.5	241	1400	317	253	0	102.3	99.6
58	11.93	257	178	2000	26.9	245	1500	309	370	0	103.2	100.6
59	10.79	158	160	644.3	22.7	84	654	89	182	0	101.7	100.8
60	10.03	161	177	655.3	23.2	85	686.1	87	200	0	102.0	101.0
61	9.07	129	219	426.5	28.8	81	270.1	97	0	94	98.8	97.7
62	8.21	131	216	428.4	29	81	270.1	90	0	99	98.6	97.4
63	12.09	0	0	4200	0.5	189	2900	363	509	0	104.3	102.3
65	11.25	7	7	168.6	0.6	13	134.4	55	62	0	100.6	100.4
67	11.14	1	0	420	0.2	107	220	111	169	0	101.6	100.3
69	13.33	905	934	641	137	176	1200	254	0	155	98.7	97.0

\*Italicized chlorine levels were estimated from P/Cl ratios.



5

Table 2  
Compositional Analyses and Charge Balance Calculations for Crystallization Mother Liquors

Example	KLG	AsA	Ca	K	Na	Ppm	P	S	Cl*	Protons/KLG, %	
	wt%	wt%				Mg				Total	Avail.
1	35.72	0	5600	11900	6900	1222	4100	1355	1681	75.2	60.9
2	19.96	0	4600	9700	5504	962	3200	1196	1312	63.6	43.5
3	21.72	1.39	60	6	24	0.6	2500	4121	1025	146.8	132.4
4	15.97	2.28	52	17	28	0.7	4400	7318	1804	213.0	178.4
5	16.47	2.81	43	12	35	0.7	6000	9874	2460	248.8	203.2
6	16.19	2.85	2	0	21	0.6	1100	20200	1815	269.9	261.4
7	14.81	3.14	0	0	12.8	0.5	2597	21200	4285	322.2	300.2
8	13.16	2	2	0	26.9	0.75	758	24000	1300	337.0	329.8
9	9.75	3.37	3	17	26	1	1261	39000	2100	620.4	604.2
10	10.6	3.21	2	8	25	0.51	1101	34000	1600	516.1	503.1
11	18.02	1.35	0	0	31	0.96	1964	15800	863	229.2	215.5
12	16.04	2.12	0	0	52	1.2	2880	23000	1200	311.3	288.8
13	12.19	4.87	0	0	68	1.7	5818	47000	2200	666.2	606.4
14	26.57	0.53	11	0	51	2	465	3809	767	122.0	119.8
15	22.25	0.93	0	0	11	0.6	650	5167	1073	136.2	132.6
16	20.22	1.67	0	0	13	0.58	839	6707	1500	152.0	146.8
17	21.36	0.44	209	14700	7209	1369	4531	20600	1900	187.7	161.1
18	22.63	0.028	181	13000	6902	1229	4200	18000	1722	171.7	148.4
19	21.78	0.34	124	17000	9495	1658	5600	25000	2296	204.9	172.7
20	21.36	0.28	205	12000	6615	1179	990	19000	1634	156.9	151.1
21	19.4	0.53	163	15900	8400	1500	1300	25100	2100	184.9	176.5
22	19.68	0.77	139	17000	9200	1600	1400	27000	2300	190.0	181.0
23	30.65	0.13	1500	11800	6600	1200	1000	3000	1700	72.7	68.6
24	32.87	0.22	1600	14700	8300	1500	1300	3400	2100	67.9	63.0
25	33.66	0.3	1600	15200	8700	1600	1400	3600	2600	68.6	63.3
26	17.01	0.86	123	342	1075	25	729	19700	1100	244.6	239.3
27	14.36	1.4	188	553	1806	41	1216	33000	2000	387.7	377.1
28	14.73	2.02	195	596	2000	44.2	1300	36100	2145	406.3	395.2
29	22.35	0.59	103	808	2021	37	2986	4748	1200	143.7	126.9
30	18.39	1.22	167	1400	3600	66	5400	8600	2200	196.7	159.8
31	18.25	1.99	207	1900	4700	85.6	7000	11100	2800	225.4	177.4
32	16.07	0.76	27	126	607.4	6.2	750	18500	1200	248.5	242.7
33	12.22	1.4	52	226	1100	11.7	1400	34400	2100	462.9	448.6
34	13.66	2.65	60	262	1300	13.4	1600	40100	2400	477.7	463.0
35	25.18	0.11	163	690	1200	124.2	19	751.6	22	97.0	96.9
36	25.92	0.69	676	2800	4800	512.1	82	3200	19	88.9	88.5
37	23.83	0.11	161	686	1100	122.5	18	737.3	34	97.2	97.1
38	27.08	0.66	685	2800	4800	514.9	81	3200	50	89.4	89.0
39	23.16	0.74	210	8400	4600	800	2700	11800	1100	145.1	130.5
40	17.44	2.41	136	20100	11300	1900	6600	28400	2600	246.5	199.1
41	22.34	0.69	222	8100	4300	762.6	2600	10700	1100	141.9	127.3
42	17.99	1.82	126	20600	11300	2000	6700	28300	2600	240.2	193.5

Table 2 continued  
Compositional Analyses and Charge Balance Calculations for Crystallization Mother Liquors

Example	KLG wt%	AsA wt%	Ca	K	Na	ppm Mg	P	S	Cl*	Protons/KLG, % Total	Avail.
43	19.48	0.61	22	228	8800	4.8	743	10900	1226	139.5	134.7
44	15.27	1.57	52	460	20200	11	1700	25100	2805	216.5	202.5
45	21.46	0.38	26	229	9300	5.1	821	6600	1300	110.5	105.7
46	20.79	0.88	90	492	20700	14.6	1800	14700	3100	124.3	113.5
47	22.09	0.43	24	225	9200	5.1	799	6500	1400	110.1	105.6
48	17.88	0.89	55	467	21400	12.2	1900	15400	3100	131.0	117.7
49	26.78	0.4	535	308	5500	51.9	960	3400	1900	105.8	101.4
50	24.68	1.27	200	882	16400	155.4	2900	9200	5600	120.0	105.3
51	25.12	0.34	525	310	5400	51.1	952	3400	1800	106.3	101.6
52	25.47	1.02	232	778	13900	132.1	2500	7800	4700	116.3	104.0
53	23.19	0	3	83	1800	0.1	1100	1800	445	112.6	106.7
54	18.10	1.51	9	262	4900	0.8	2800	4600	932	139.1	119.7
55	23.13	0.5	3	86	1800	0.4	1000	1700	428	111.3	105.9
56	19.98	1.27	7	216	4200	0.6	2300	3900	983	129.7	115.2
57	23.29	0.34	190	1300	15300	204	1900	9700	2400	111.0	100.8
58	23.11	0.37	193	1300	14800	198	1800	9600	2300	111.4	101.6
59	23.67	0.4	237	1100	4500	160.3	579	4000	623	106.1	103.0
60	25.11	0.44	242	1200	4600	163.2	598	4100	644	105.8	102.9
61	30.52	0	729	2100	4200	285.1	805	2300	861	96.8	93.5
62	28.25	0.37	738	2000	3900	270	764	2200	827	96.9	93.5
63	21.97	0.6	19	0	25000	5.6	1100	17100	2000	112.5	106.2
64	23.70	0.94	30	0	35600	4.2	1700	25600	3300	125.0	116.0
65	24.69	0.41	46	0	878	2.9	79	806	334	102.1	101.7
66	22.78	0	221	55	3900	12.9	351	3600	1500	110.0	108.1
67	24.46	0.92	8	0	2800	1	719	1600	755	105.4	101.8
68	15.61	1.62	20	0	6700	2.2	1700	3800	1800	119.9	106.2
69	26.12	0.02	615	4400	3100	665	874	3000	1300	98.2	94.0
70	27.82	0.82	622	10400	7200	1600	2100	6700	3100	97.7	88.2

\*Italicized chlorine levels were estimated from P/Cl ratios.

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Table 3  
Compositional Analyses and Charge Balance Calculations for Pretreated Feeds Before Final Protonation Step

Example	KLG wt%	Ca	K	Na	ppm Mg	P	S	Cl*	Implied, ppm H <sub>3</sub> O <sup>+</sup>	OH <sup>-</sup>	Protons/KLG, % Total	Avail.
45A	11.05	4	24	105.6	1.1	118	890.2	<i>194.7</i>	1274	0	111.77	110.4
45B	10.59	4	40	90.3	0.6	117	884.4	<i>193.1</i>	1270	0	112.24	110.9
45C	10.44	3	39	80	0.4	114	865.1	<i>188.1</i>	1249	0	112.21	110.8
49A	15.07	42	36	63	4.7	181	576	<i>314.0</i>	1069	0	107.2	105.7
49B	15.47	157	75	172.5	14.8	184	576	<i>319.2</i>	842	0	105.6	104.1
57	11.07	263	184	390	27.6	249	1500	316	1704	0	115.7	112.9
63	12.49	0	0	47.9	0.5	189	2800	373	3831	0	131.3	129.4
69	14.05	2000	766	572	116	150	539	253	0	1676	86.4	85.0

\*Italicized chlorine levels were estimated from P/Cl ratios.

While the present invention has been described in terms of certain embodiments thereof, it will be recognized that various substitutions, modifications, alterations, omissions and other changes may be made without departing from the spirit thereof.

10 Accordingly, the scope of the present invention is to amend only by the scope of the following claims, including equivalents thereof.

**What is claimed is:**

1. A process for recovering a desired organic acid from a solution comprising the steps of:
  - (a) providing an aqueous solution comprising at least one desired organic acid or its acid anion;
  - (b) adjusting the proton concentration in the aqueous solution to a desired level, with the desired proton concentration being selected, at least in part, by the amount of available protons needed to associate with the acid anions of the desired organic acid(s) and/or acid anions that are weaker than the desired organic acids; and
  - (c) recovering at least a portion of the at least one desired organic acid from the aqueous phase.
2. The process according to claim 1 wherein the desired proton concentration is based on the amount of available protons being substantially equal to the amount of protons needed to associate with the anion of the desired organic acid(s) and acid anions that are weaker than the desired organic acid(s).
3. The process according to claim 1 wherein the desired proton concentration is based on the amount of available protons being greater than the amount of protons needed to associate with the anions of the desired organic acid(s) and acid anions that are weaker than the desired organic acid(s).
4. The process according to claim 3 wherein the desired proton concentration is based on an amount of protons that is about 1 to about 10 % greater than the amount of protons needed to associate with the desired organic acid(s) and acid anions that are weaker than the desired organic acid(s).
5. The process according to claim 1 wherein the desired proton concentration is based on the amount of available protons being less than the amount of protons

needed to associate with the anions of the desired organic acid(s) and acid anions that are weaker than the desired organic acid(s).

6. The process according to claim 5 wherein the desired proton concentration is based on an amount of protons that is about 1 to about 10% less than the amount of protons needed to associate with the desired organic acid(s) and acid anions that are weaker than the desired organic acid(s).
7. The process according to claim 1 wherein the at least one desired organic acid is an acid in which the salt form of the organic acid is more soluble in water than the acid itself.
8. The process according to claim 1 wherein the at least one desired organic acid is susceptible to acid catalyzed decomposition.
9. The process according to claim 1 wherein the at least one desired organic acid is selected from the group consisting of ascorbic, succinic, tartaric, glyconic, gluconic gulonic, citric, lactic, malic, maleic, acetic, formic, pyruvic, propionic, butyric, itaconic acids and mixtures thereof.
10. The process according to claim 1 wherein the at least one desired organic acid is a carboxylic acid.
11. The process according to claim 1 wherein the at least one desired organic acid is an alkali or alkaline earth salt form.
12. The process according to claim 11 wherein a counter ion is sodium, potassium or calcium.
13. The process according to claim 1 wherein the at least one desired organic acid is at least partially present in an ammonium form.

14. The process according to claim 1 wherein the at least one desired organic acid is at least partially present in its anionic form.
15. The process according to claim 1 wherein the aqueous solution further includes additional acid anions.
16. The process according to claim 1 wherein the additional acid anions are selected from among phosphates, sulfates, nitrates, and chlorides.
17. The process according to claim 1 wherein the aqueous solution comprises a fermentation broth that includes unreacted sugar.
18. The process according to claim 1 wherein the adjusting step (b) comprises (i) introducing at least one acid into the aqueous solution.
19. The process according to claim 18 wherein the at least one acid is a strong acid as compared to the organic acid(s) being recovered.
20. The process according to claim 18 wherein the acid is selected from among sulfuric, hydrochloric, nitric and phosphoric acids.
21. The process according to claim 18 wherein the amount of acid introduced in step (b), (i) is that amount effective to convert at least a portion of any organic acid salt(s) present in the aqueous solution to their acid form.
22. The process according to claim 21 further comprising step (b) (ii) removing at least a portion of any precipitated salts produced in step (i).
23. The process according to claim 22 further comprising step (b) (iii) contacting the aqueous solution with a cation exchange resin in its hydrogen or acid form.

24. The process according to claim 23 wherein the cation exchange resin comprises a sulfonated polystyrene resin.
25. The process according to claim 23 wherein the adjusting step further comprises step (b) (iv) introducing at least one base in an amount effective to neutralize at least a portion of any strong acid(s) formed by step (iii).
26. The process according to claim 25 wherein the base is selected from among sodium hydroxide and potassium hydroxide.
27. The process according to claim 25 wherein the base is the salt form of the organic acid(s) to be recovered.
28. The method according to claim 1 further comprising recycling at least a portion of a stream recovered from step (c) to a point before or during step (b).
29. The process according to claim 27 wherein the recycle is contacted with an anion exchange resin before introduction into the aqueous solution.
30. The method according to claim 28 further comprising recycling at least a portion of a stream recovered from step (c) to a point after step (b) (i).
31. The method according to claim 22 further comprising recycling at least a portion of a stream recovered from step (c) to a point after step (b) (ii).
32. The process according to claim 1 wherein the adjusting step comprises (i) contacting the aqueous solution with a cation exchange resin in its hydrogen or acid form.
33. The process according to claim 31 wherein the cation exchange resin comprises a sulfonated polystyrene resin.

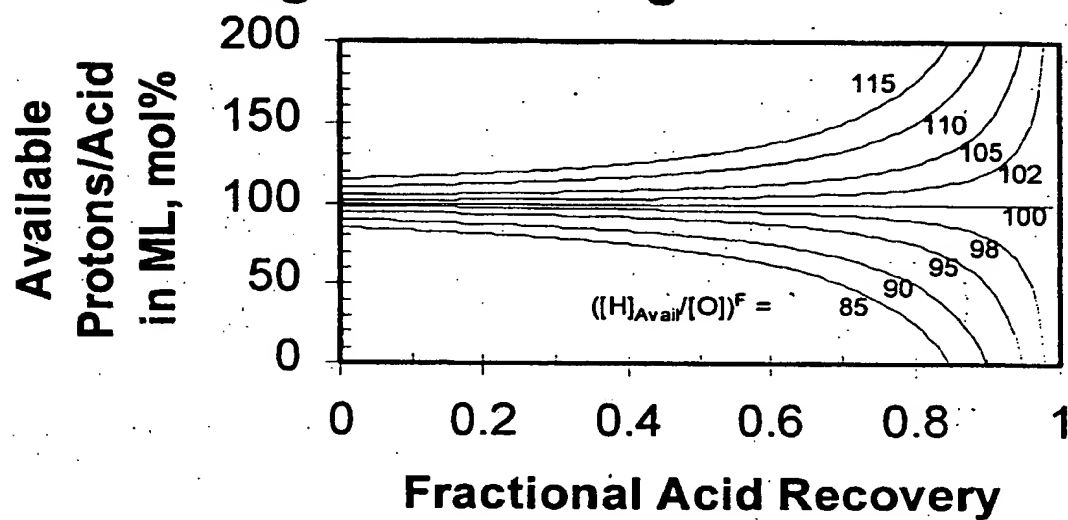
34. The process according to claim 31 wherein the adjusting step further comprises (ii) introducing at least one base in an amount effective to neutralize at least a portion of any strong acid(s) formed by step (i).
35. The process according to claim 33 wherein the base is selected from among sodium hydroxide and potassium hydroxide.
36. The process according to claim 33 wherein the base is the salt form of the organic acid(s) to be recovered.
37. The process according to claim 33 further comprising recycling at least a portion of a stream recovered from step (c) to a point after step (b) (i).
38. The process according to claim 36 wherein the recycle is contacted with an anion exchange resin before introduction into the aqueous phase.
39. The process according to claim 1 wherein step (c) comprises isolating the at least one desired organic acid(s).
40. The process according to claim 39 wherein the isolation step comprises both (i) crystallizing the desired organic acid(s) from the aqueous solution, and (ii) at least one of filtration, decantation, centrifugation, extraction, and/or spray drying.
41. The process according to claim 40 further comprising recycling at least a portion of a stream recovered from step (c)(ii) for introduction into the aqueous solution.
42. The process according to claim 41 wherein the recycle is contacted with an anion exchange resin before introduction into the aqueous solution.



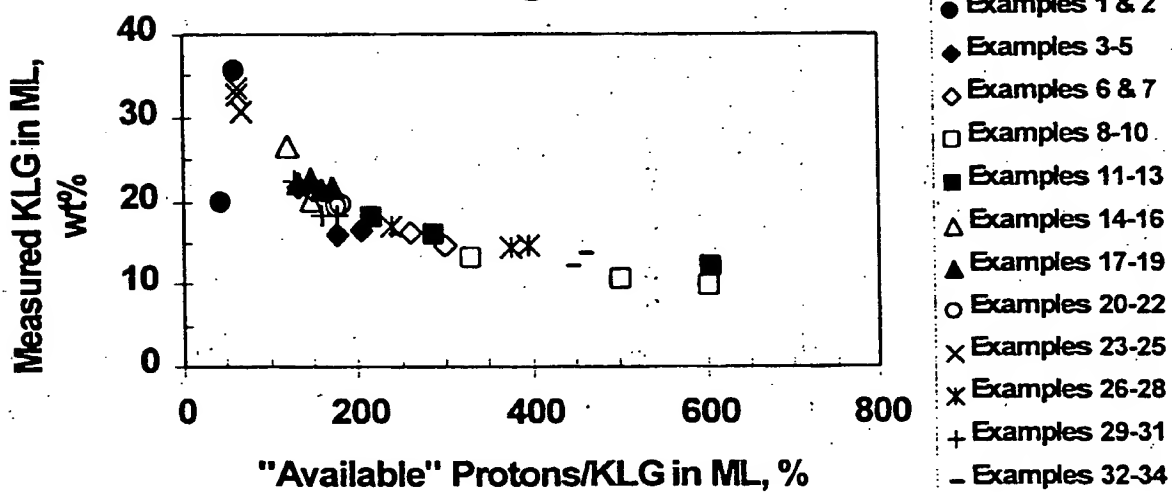
43. The process according to claim 1 wherein the organic acid is 2-keto-L-gulonic acid or 2-keto-D-gluconic acid.
44. The process according to claim 43 wherein step (a) comprises producing the 2-keto-L-gulonic acid or 2-keto-D-gluconic acid by a fermentation reaction.
45. The process according to claim 44 wherein the fermentation reaction is performed in the presence of at least one organism and/or enzyme.
46. The process according to claim 43 further comprising (d) converting the 2-keto-L-gulonic acid or 2-keto-D-gluconic acid to ascorbic acid and/or erythorbic acid.
47. The process according to claim 1 wherein the process does not include contacting the aqueous solution with an anion exchange resin.
48. The process according to claim 1 wherein determination of the desired proton concentration includes titration in an aprotic solvent.
49. The process according to claim 48 wherein the aprotic solvent is DMSO.
50. The process according to claim 49 further comprising the addition of at least one salt which can precipitate at least a portion of sulfate present in the solution while replacing the sulfates with an acid anion stronger than the at least one desired organic acids.
51. The process according to claim 50 wherein the at least one salt is a barium, magnesium or strontium salt.

52. The process according to claim 51 wherein the salt is barium chloride, barium perchlorate, barium bromide; magnesium perchlorate, or mixtures thereof.
53. An organic acid produced by the process of claim 1.
54. A composition comprising an aqueous solution containing 2-keto-L-gulonic acid and a predetermined proton concentration that is substantially equal to the amount of protons needed to associate with the 2-keto-L-gulonic acid and acid anions that are weaker than 2-keto-L-gulonic acid.
55. A composition comprising an aqueous solution containing 2-keto-L-gulonic acid and a predetermined proton concentration that is greater than the amount of protons needed to associate with the 2-keto-L-gulonic acid and acid anions that are weaker than 2-keto-L-gulonic acid.
56. The composition according to claim 55 wherein the predetermined proton concentration is about 1 to about 10% greater than the amount of protons needed to associate with the 2-keto-L-gulonic acid and acid anions that are weaker than 2-keto-L-gulonic acid.
57. A composition comprising an aqueous phase containing 2-keto-L-gulonic acid and a predetermined proton concentration that is less than the amount of protons needed to associate with the 2-keto-L-gulonic acid and acid anions that are weaker than 2-keto-L-gulonic acid.
58. The composition according to claim 57 wherein the predetermined proton concentration is about 1 to about 10% less than the amount of protons needed to associate with the 2-keto-L-gulonic acid and acid anions that are weaker than 2-keto-L-gulonic acid.

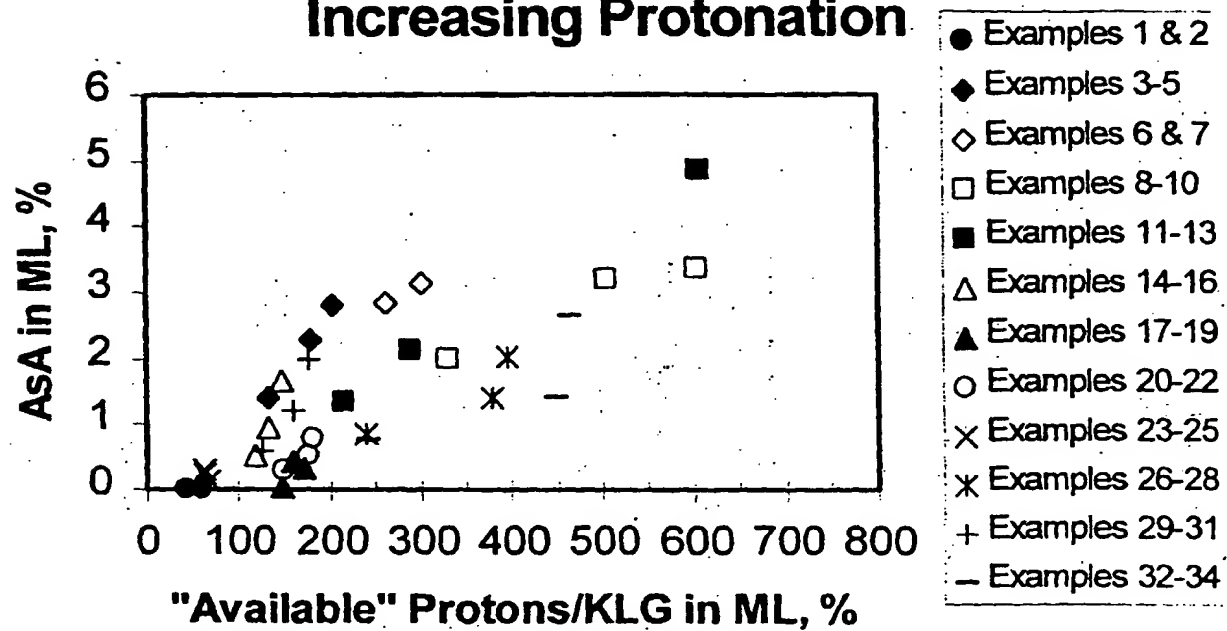
**Figure 1 - Improper Protonation is Magnified During Acid Recovery**



**Figure 2 - Solubility Decreases with Increasing Protonation**



**Figure 3 - AsA in ML Increases with Increasing Protonation**



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